## THERMODYNAMICS

## $\square \quad$ What is Thermodynamics and why is it useful ?

Thermodynamics is the branch of science that describes the behaviour of matter and the transformation between different forms of energy on a macroscopic scale. Thermodynamics describes a system in terms of its bulk properties. Only a few such variable are needed to describe the system, and the variables are generally directly accessible through measurements. A thermodynamic description of matter does not make reference to its structure and behaviour at the microscopic level.

- The laws of Thermodynamics :

The law's of thermodynamics is the law of observation. No one has ever observed that any thing goes in contrary to thermodynamics law. So we elevate this observation to the status of thermodynamic law. The real justification of this comes when things we derive using this law turn's out to be true that is verified by experiments :

## - Application of Thermodynamics :

(i) It provides relationship between heat, work and measurable properties of matter.
(ii) It predicts direction of natural change - like what circumstances are best for rusting of iron.
(iii) It predicts up to what extent a chemical reaction can proceed in forward direction.

Example : How much ammonia $\left(\mathrm{NH}_{3}\right)$ can be formed from $\mathrm{N}_{2}$ and $\mathrm{H}_{2}$ in a closed container.
(iv) It help in understanding why different phases of matter exist - and provide simple relationship between various measurable properties of system (thermodynamical variables) :

## - Salient featurs of Thermodynamics :

During study of this chapter you will observe that mostly you will be dealing with macroscopic properties (bulk properties) like pressure, volume, temperature density of system. This is because thermodynamics is macroscopic science and it do not concern's with detailed microscopic make up of the system.

## - Limitations

(1) It tells us whether a given chemical reaction will take place or not under the given set of conditions but doesn't tell us anything about the rate of reaction.
(2) It tells us about the initial and final properties of the system but doesn't tell us anything about the path or mechanism followed by the system.

## $\square$ Basic definitions :

(i) System : Part of universe under investigation is called system.
(ii) Surrounding : Anything out side the system is called surrounding.

- Types of system :
(i) Closed system : A system which can exchange only energy with surrounding.
(ii) Open system : A system which can exchange both energy and matter with surrounding.
(iii) Isolated system : A system which cannot exchange matter or energy with surrounding.
(iv) Homogeneous system : System consist of single phase. eg. Pure solid, a pure liquid a solution, or a mixture of gases.
(v) Heterogenous system : A system consisting of many phases. eg. System of two immiscible liquids, two or more solids, a liquid in contact with its vapour etc. are example of heterogenous system.
(vi) Boundary: The interface between system and surrounding is called boundary. Across boundary energy and mass are transferred between system and surrounding. Boundary can be real or hypothetical.
(vii) Wall : A real boundary is called wall can be rigid,
- Types of wall:

Rigid wall : The wall is immovable $\Rightarrow \mathrm{w}_{\mathrm{PV}}=0$.
Non Rigid wall : The wall is movable $\Rightarrow \mathrm{w}_{\mathrm{PV}} \neq 0$.
Adiabatic wall : The heat exchange across the wall is $\mathrm{q}=0$.
Dithermic wall : The heat can be exchanged across the wall $\Rightarrow \mathrm{q} \neq 0$.
Phase : By the term phase we mean a homogeneous physically distinct part of a system which is bounded by a surface and can be separated out mathematically from the other parts of the system.

## The state of a system :

We specify the state of a system - say, a sample of material - by specifying the values of all the variables describing the system. If the system is a sample of a pure substance this would mean specifying the values of the temperature, T , the pressure, p , the volume, V , and the number of moles of the substance, n .
State variables : To define a thermodynamics states of a system, we have to specify the values of certain mesurable quantities. These are called thermodynamic variable or state variable.
A system can be completely defined by four variables namely pressure, temperature, volume and composition. A system is said to be in a certain definite state when all of its properties have definite value.. Between two fixed state the change in the value of state function is same irrespective of the path connection two states.
Differential of a state function integerated over a cyclic path returns zero. In other words summation of change in state function in a cyclic process is equal to zero.

$$
\text { if } \quad \oint \mathrm{dX}=0 \Rightarrow \mathrm{X} \text { is a state function (property of state function) }
$$

note that if X is a state function, dX is called definite quantity
Example : T, V, P and U (internal energy), H (enthalpy) are state variables.

- EXAMPLE BASED ON BASIC DEFINITION :

1. Which one is not a state function :-
(A) internal energy
(B) volume
(C) heat
(D) enthalpy

Ans. (C)
2. When no heat energy is allowed to enter or leave the system, it is called :-
(A) isothermal process
(B) reversible process
(C) adiabatic process
(D) irreversible process

Ans. (C)
3. Which is the intensive property :-
(A) temperature
(B) viscosity
(C) density
(D) all

Ans. (D)
4. A thermodynamic state function is :-
(A) one which obeys all the law of thermodynamics
(B) a quantity which is used in measuring thermal changes
(C) one which is used in thermo chemistry
(D) a quantity whose value depends only on the state of system

Ans. (D)
5. A system is changed from state3 $A$ to state $B$ by one path and from $B$ to $A$ by another path. If $\Delta \mathrm{E}_{1}$ and $\Delta \mathrm{E}_{2}$ are the corresponding changes in internal energy, then :-
(A) $\Delta \mathrm{E}_{2}+\mathrm{E}_{2}=+\mathrm{ve}$
(B) $\Delta \mathrm{E}_{1}+\Delta \mathrm{E}_{2}=-\mathrm{ve}$
(C) $\Delta \mathrm{E}_{1}+\Delta \mathrm{E}_{2}=0$
(D) none of the above

Ans. (C)
6. A well stoppered thermos flask contains some ice cubes. This is an example of a :-
(A) closed system
(B) open system
(C) isolated system
(D) non-thermodynamics system

Ans. (C)

## Path function or path dependent quantities :

The value of path function depends upon path connection two states. There can be infinite vaules of path function between two states depending upon path or process.
Path functions are also called indefinite quantities since between two fixed state the value of path function is not fixed. Heat and Work are two important path dependent quantities with which we deal in this chapter.

## - Extensive and Intensive variables :

Propterties which depend on the amount of the substance (or substances) present in the system are called extensive propterties. e.g. Mass, volume, heat capacity, internal energy, entropy, Gibb's free energy (G), surface area etc. These properties will change with change in the amount of matter present in the system. It is important to note that the total value of an extensive property of a system is equal to the sum of the values of different parts into which the system is divided.

Intensive properties : Properties which are independent of the amount of substance (or substances) present in the system are called intensive properties, e.g. pressure, density, temperature, viscosity, surface tension, refractive index, emf, chemical potential, sp . heat etc, These are intensive properties.

An extensive property can be converted into intensive property by defining it per unit of another extensive property.
Ex. Concentration $=$ mole $/$ volume
Density = mass / volume
heat capacity $=$ heat absorbed $/$ rise in temperature
While mole, mass, heat are extensive properties, concentration, density and heat capacity are intensive properties.

## - Thermodynamic equilibrium :

Thermodynamic generally deals the equilibrium state of the system in which the state variable are uniform and constant throughout the whole system.
The term thermodynamic equilibrium implies the existence of three different types of equilibria in the system. These are :
(i) Mechanical equilibrium :

When there is no macroscopic movement within the system itself or of the system with respect to surroundings, the system is said to be in a state of mechanical equilibrium.
(ii) Chemical equilibrium :

When the system consists of more than one substance and the composition of the system does not vary with time, the system is said to be in chemical equilibrium. The chemical composition of a system at equilibrium must be uniform and there should be no net chemical reaction taking place.
(iii) Thermal equilibrium :

When the temperature throughout the entire system is the same as that of the surroundings then the system is said to be in thermal equilibrium.

## $\square$ Equation of state :

An equation that relates the variables $\mathrm{T}, \mathrm{p}, \mathrm{V}$, and n to each other is called the "equation of state." The most general form for an equation of state is.

$$
f(\mathrm{p}, \mathrm{~V}, \mathrm{~T}, \mathrm{n})=0
$$

## $\square \quad$ The ideal gas equation of state :

The best known equation of state for a gas is the "ideal gas equation of state". It is usually written in the form,

$$
\mathrm{pV}=\mathrm{nRT}
$$

This equation contains a constant, R , called the gas constant.

- The vander Walls equation of state for real gases :

The vander Walls equation of state is,

$$
\left(p+a \frac{n^{2}}{V^{2}}\right)(V-n b)=n R T
$$

Notice that the vander Walls equation of state differs from the ideal gas by the addition of two adjustable parameters, $a$, and $b$ (among other things).
Note : Equation of state for liquid and solids are also defined empirically.

- Process : Anything which changes state of system is called process. Usually as a result of heat and work interactions change of state take place. e.g. isothermal process
$\square$ Path of a process : The exact sequence of steps through which system changes state is called path of a process.e.g. reversible or irrervisible path

Some thermodynamic processes :
(1) Isothermal process : A process in which temperature of the system remains constant is called isothermal process.
(2) Isobaric process : A process in which pressure of the system remains constant is called isobaric process. Temperature and volume of the system may change.
Ex. All the reactions or processes taking place in open vessel like boiling of water in open vessel, burning of charcoal, melting of wax take place at contant pressure (1 atm.)
(3) Adiabatic process : A process in which no heat exchange takes place is called adiabatic process. Adiatatic process occurs in isolated systems.
(4) Isochoric process : The process for which volume of the system remains constant is called isochoric process i.e., Heating of gas in closed vessel.
(5) Cyclic process : If a system after completing a series of different process returns to its initial state then overall process is called cyclic process.
In cyclic process all the state variables remains constant because initial state becomes final state in cyclic process.
Ex. $\Delta \mathrm{H}=0, \Delta \mathrm{E}=0, \Delta$ P.E. $=0$

- Polytropic processes : It is defined as a process in which $\mathrm{PV}^{\mathrm{n}}=$ constant $=\mathrm{k}$

All of the above mentioned processes can be performed in two ways, reversibly and irreversibly

- Reversible process : When the difference between driving force and opposing force is very small and the process is carried out infinitesimally slowly, then the process is called reversible process. The reversible process is carried out in such a manner that at any moment of the change the directon of process can be reversed by making a small change in driving force.A reversible process is also called quasi static process. During a reversilbe process, the system and surrounding remain in equilibrium throught the process.

The reversible proceses are idealized processes which cannot be actually carried out, but neverthless they are very important because they help in calculation of change in state function in the process.In other words the reversible processes are hypothetical processes.
A quasi static process is the one in which system remain infinitesimally closer to the state of equilibrim through out the process.

- Irreversible process : Any process which does not take place in the above manner and difference between driving force and the opposing force is quite large is called irreversible process.All natural processes are example of irreversible process.

| Reversible process |  | Irreversible process |  |
| :---: | :---: | :---: | :---: |
| (1) | Driving force is infinitesimally small. | (1) | Driving force is large and finite. |
| (2) | PV work is done across pressure difference d P | (2) | PV work is done across pressure difference $\Delta \mathrm{P}$ |
| (3) | A reversible heat transfer take place across temperature difference dT | (3) | Irrerversible heat transfer take place across temperatur difference $\Delta \mathrm{T}$ |
| (4) | It is an ideal process. | (4) | It is a real process. |
| (5) | It takes infinite time for completion of process. | (5) | It takes finite time for completion of process.. |
| (6) | It is an imaginary process and can not be realised in actual practice. | (6) | It is a natural process and occurs in particular direction under given set of conditions. |
| (7) | Throughout the process, the system remain infinetesimelly closer to state of equilibrium and exact path of process can be drawn | (7) | The system is far removed from state of equilibrium and exact path of process is indeterminate. |

## - Heat and Work :

Heat and work both are mode of energy transfer between system and surrounding.
Heat flows due to temperature gradient while work is done due to imbalance of generalized force. Due to imbalance of generalized force(intersive property) generalized displacement (extensive property) is produced. The product of generalized force and generalized displacement is work.
Work done on the system can reversible and irrervisible depending on magnitude of imbalance of generalized force.
Heat is also transfered between system and surrounding in two ways - reversible and irreversible.
Reverssible heating means heating an object from $T_{i}$ to $T_{f}$ using infinite heat reservoirs.
Irreverssible heat transfer means heat transfer across temp difference $\Delta \mathrm{T}$.
Heating an object from 100 K to 1000 K by using heat reservoir of temperature 1000 K is an example of irreverssible heating.

While heating an object from 100 to 1000 K using reservoir of temp $100+\mathrm{dT}, 100+2 \mathrm{dT}, \ldots \ldots \ldots$ $1000-\mathrm{dT}, 1000 \mathrm{~K}$ is an example of reversible heating. You can clearly see reversible heating is hypothetical concept.

Work can be of many types :
The following table show different kinds of work.

| Type of Work | Variables | Equation for Work | Conventional <br> Units |
| :---: | :---: | :---: | :---: |
| Volume expansion | Pressure (P), volume (V) | $\mathrm{w}=-\int P_{\text {external }} \mathrm{dV}$ | $\mathrm{Pa} \mathrm{m}^{3}=\mathrm{J}$ |
| Stretching | Tension ( $\gamma$ ), length (l) | $\mathrm{w}=-\int \gamma \mathrm{dl}$ | $\mathrm{N} \mathrm{m}=\mathrm{J}$ |
| Surface expansion | Surface tension $(\gamma)$, area ( $\sigma$ ) | $\mathrm{w}=-\iint \gamma \mathrm{d} \sigma$ | $\left(\mathrm{N} \mathrm{m}^{-1}\right)\left(\mathrm{m}^{2}\right)=\mathrm{J}$ |
| Electrical | Electrical potential $(\phi)$, | $\mathrm{w}=-\int \phi \mathrm{dq}$ | $\mathrm{V} \mathrm{C}=\mathrm{J}$ |

$\square \quad$ PV-WORK Consider a clylinder fitted with a frictionless piston, which enclosed $n$ mole of an ideal gas. Let an external force $F$ pushes the piston inside producing displacement in piston.Let distance of piston from a fixed point is x and distance of bottom of piston at the same fixed point is $\ell$. This means the volume of cylinder $=(\ell-x) \mathrm{A}$ where A is area of cross section of piston.


- For a small displacement dx due to force F , work done on the system.

$$
\mathrm{dw}=\mathrm{F} . \mathrm{dx}
$$

Also $\quad P=\frac{F}{A}$
$F=P A$
$\mathrm{dW}=$ PA. dx
$\mathrm{V}=(\ell-\mathrm{x}) \mathrm{A}$
$\Rightarrow \quad d V=-A . d x$
$\Rightarrow \quad d W=-P_{\text {ext. }} d V$
Note: During expansion dV is +ive and hence sign of w is -ive since work is done by the system and -ive sign representing decrese in energy content of system. During compression, the sign of dV is -ive which gives +ive value of $w$ representing the increase in energy content of system during compression.
$\square$ SIGN CONVENSIONS :

- According to latest sign conventions
(a) Work done is taken negative if it is done by the system since energy of system is decreased.

Ex. Expansion of gas.
(b) Work done is taken positive if it is done on the system, since energy of system is increased.
$\therefore \quad \mathrm{W}=-\mathrm{P}_{\mathrm{ex}} . \Delta \mathrm{V}$
Q. Find the work done in each case :
(a) When one mole of ideal gas in 10 litre container at 1 atm . is allowed to enter a vaccuated bulb of capacity 100 litre.
(b) When 1 mole of gas expands from 1 litre to 5 litre against constant atmospheric pressure.
A. (a) $W=-P \Delta V$

But since gas enters the vaccum bulb and pressure in vaccum is zero. This type of expansion is called free expansion and work done is zero.

Note : Work done in free expansion is always zero.
(b) $\mathrm{W}=-\mathrm{P} \Delta \mathrm{V}=-1(5-1)=-4$ litre-atm.
Q. Find the work done when 18 ml of water is getting vapourised at 373 K in open vessel (Assume the ideal behaviour of water vapour).
A.

$$
\begin{array}{rlrl}
\mathrm{PV} & =\mathrm{nRT} & \text { [V in litre and T in Kelvin }] \\
\mathrm{PV} & =1 \quad 0.0821 & \\
\mathrm{PV} & =30 \text { litre } & \\
\mathrm{V} & =30 \text { litre } & \\
\mathrm{W} & =-\mathrm{P} \Delta \mathrm{~V}=1 \mathrm{~atm} .] \\
& =-1\left(30-\mathrm{V}_{\text {gas }}\right) & {[18 \mathrm{ml} \text { is negligible as compared to } 30 \text { litre }]} \\
& =-1 \quad 30=-30 \text { litre atm. }
\end{array}
$$

- Heat : Heat is defined as the amount of energy which flows between system and surrounding because of temperature difference.
Note : Heat always flows from high temperature to low temperature .
- Sing convention :
- Heat is taken negative when it goes out of the system.
- Heat is taken positive when it comes inside the system.


Difference between heat and work :
When a gas is supplied some heat, its molecules move faster and with greater randomness in different directions. But when work is done on the same system gas molecules are compressed and move initially in direction of force as they get condensed.
So heat is random form of energy while work is organised from of energy.

- The internal energy and the first law of thermodynamics :

The first law of thermodynamics is based on experience that energy can be neither created nor destroyed, if both the system and the surroundings are taken into account.Suppose a blocks of mass ' M ' is moving in gravitational field with velocity v. The total energy of blocks (in earth frame of reference) is given as :

$$
E=K+V+U:(K=\text { kinetic energy, } V=\text { potential energy, } U=\text { internal energy })
$$

A thermodynamic system is studies generally at rest so $K=0$. If effect of gravitation field (or other fields are ignored) is also ignored then we left with $E=U$. Thus $U$ (internal energy) is energy of system.

If a system is present in particular thermodynamic state say ' $A$ ' it has fixed amount of internal energy $U_{A}$. Suppose by a process the system is taken from state A to state B. In the process 'q' heat is absorbed by system and w work is done on the system. Thus in the state ' B ' total internal energy of system become

$$
\begin{aligned}
& U_{B}=U_{A}+q+w . \\
& U_{B}-U_{A}=q+w \\
\Rightarrow & \Delta U=q+w
\end{aligned}
$$

This is mathematical statement of first law.

First law of thermodynamics states that energy is conserved. Direct consequence of this statement is $U$ is state function. This implies between any two fixed state, there can be infinite process or path, but $\Delta U$ in all process will remain the same.(Property of a function of state)
Consider a system taken from state $A$ to $B$ by $n^{\text {th }}$ different paths.


Here $\mathrm{q}_{\mathrm{i}}$, $\mathrm{w}_{\mathrm{i}}$ are heat and work involve in respective processes.

- Note that heat and work involve in all the process are different but $\Delta U$ is same. This mean heat and work are indefinite quantities while $\Delta U$ is a definite quantity.
$\Rightarrow \quad$ Some other statement of first law :

$$
\left.\sum_{\substack{\text { cyclic } \\ \text { process }}} \Delta \mathrm{U}=0=\text { or } \oint \mathrm{dU}=0 \quad \text { \{Integral of } \mathrm{dU} \text { over cyclic path is zero. }\right\}
$$

First law of thermodynamics applied to close system involving only PV work.
For system involving only PV work first law mathematical statement can be written in differential from as :

$$
\mathrm{dU}=\mathrm{dq}-\mathrm{PdV}
$$

The microscopic nature of First law of thermodynamics:
The internal energy of the gas confined in a container is defined relative to a coordinate system fixed on the container. Viewed at a microscopic level, the internal energy can take on a number of forms such as.

- The kinetic energy of the molecules ;
- The potential energy of the constituents of the system; for example, a crystal consisting of dipolar molecules will experience a change in its potential energy as an electric field is applied to the system ;
- The internal energy stored in the form of molecular vibrations and rotations;
- The internal energy stored in the form of chemical bonds that can be released through a chemical reaction.

The total of all these forms of energy for the system of interest is given the symbol $U$ and is called the internal energy.

Hence total internal energy of a system can be written as
$U=U_{\text {translational }}+U_{\text {rotational }}+\mathrm{U}_{\text {vibrational }}+\mathrm{U}_{\text {intermolecular }}+\mathrm{U}_{\text {electronic }}+\mathrm{U}_{\text {relativistic }}$
of these $U_{\text {relativistic }}$ and $U_{\text {eletronic }}$ is unaffected by ordinary heating. So basically the kinetic energy terms and $U_{\text {intermolecur }}$ accommodate heat provided to the system. Hence heat capacity of a sample depends upon these four terms.

For an ideal gas, $U_{\text {intermolecular }}$ is equal to zero, because of absence of intermolecular force of attraction in ideal gas. $\mathrm{U}_{\text {intermolecular }}$ have large and negative value in solids and liquids.
For an ideal gas $U$ is only function of temperature e.g. $U=F(T)+$ Constant
Due to absence of pressure or volume terms in ideal gas internal energy, $U$ is independent of pressure and volume of theoretical ideal gas.

Chemical reactions are generally carried out at constant pressure (atmospheric pressure) so it has been found useful to define a new state function Enthalpy (H) as :

$$
H=U+P V \text { (By definition) }
$$

or $\quad \Delta \mathrm{H}=\Delta \mathrm{U}+\Delta(\mathrm{PV})$
or $\quad \Delta \mathrm{H}=\Delta \mathrm{U}+\mathrm{P} \Delta \mathrm{V}$ (at constant pressure) combining with first law. Equation (1) becomes

$$
\Delta H=q_{p}
$$

Heat exchange at constant volume and constant pressure ( $\mathrm{q}_{\mathrm{p}}$ and $\mathrm{q}_{\mathrm{v}}$ ):
For an isochoric process in a system involving only PV work,

$$
\Delta \mathrm{U}=\mathrm{q}_{\mathrm{V}}
$$

This result is valid for all the substance under isochoric conditions (when only PV work is involved) Also from the previous article it is clear that

$$
\Delta H=q_{p}
$$

This result is valid for all the substance involving isobaric process(when only PV work is involved)
Hence heat exchanged at constant pressure and volume are important Definite quantities
Heat capacity :
The heat capacity of a system may be defined as the amount of heat required to raise the temperature of the system by one degree.

If $\delta \mathrm{q}$ is the small quantity of heat added to the system, let the temperature of the system rises by dT , then heat capacity C of the system is given by

$$
\begin{equation*}
\mathrm{C}=\frac{\mathrm{dq}}{\mathrm{dT}} \tag{i}
\end{equation*}
$$

In case of gases we have two types of heat capacity i.e. heat capacity at constant volume and heat capacity at constant pressure.

Heat capacity at constant volume ( $\mathrm{C}_{\mathrm{v}}$ ) :
Molar heat capacity at constant volume is defined by the relation

$$
\begin{equation*}
\mathrm{C}_{\mathrm{V}}=\frac{\mathrm{dq}_{\mathrm{v}}}{\mathrm{dT}} \tag{ii}
\end{equation*}
$$

For first law of thermodynamics

But $\quad d w=P d V$
$\therefore \quad d U=d q-P d V$
At constant volume

$$
\mathrm{dU}=\mathrm{dq}_{\mathrm{v}}
$$

$\therefore$ Heat capacity at constant volume $\mathrm{C}_{\mathrm{v}}$ is given by

$$
\begin{array}{ll}
\mathrm{C}_{\mathrm{v}}=\frac{\mathrm{dq}_{\mathrm{v}}}{\mathrm{dT}}=\left(\frac{\partial \mathrm{U}}{\partial \mathrm{~T}}\right)_{\mathrm{v}} \\
\text { or } & \mathrm{C}_{\mathrm{v}}=\left(\frac{\partial \mathrm{U}}{\partial \mathrm{~T}}\right)_{\mathrm{v}} \tag{iv}
\end{array}
$$

It may be defined as the rate of change of internal energy with temperature at constant volume.

Heat capacity at constant pressure $\left(\mathrm{C}_{\mathrm{p}}\right)$ :
When pressure is maintained constant, equation (i) takes the form

$$
\begin{equation*}
C_{p}=\frac{\delta q_{v}}{d T} \tag{v}
\end{equation*}
$$

From first law of thermodynamics

At constant pressure

$$
\begin{align*}
& \delta q_{p}=(d U+P d V)=d H \\
& {[\because H=U+P V \text { At constant } P, d H=d U+P d V]} \tag{vi}
\end{align*}
$$

$\therefore \quad \delta \mathrm{q}_{\mathrm{p}}=\mathrm{dH}$
Heat capacity at constant pressure $C_{p}$ is given by

$$
\begin{align*}
& C_{p}=\frac{\delta d_{p}}{d T}=\left(\frac{\partial H}{\partial T}\right)_{P} \\
& C_{p}=\left(\frac{\partial H}{\partial T}\right)_{P} \tag{vii}
\end{align*}
$$

It is the rate of change of enthalpy with temperature at constant pressure.
Hence heat capacity of a system at constant volume $C_{v}$ is equal to the increase in internal energy of the system per degree rise of temperature at constant volume. Similarly heat capacity at constant pressure $C_{p}$ is numerically equally to the increase in enthalpy of the system per degree rise of temperature.

For 1 mole of an ideal gas, heat capacity at constant pressure i.e. $C_{p}$ is greater than the heat capacity at constant volume i.e., $\mathrm{C}_{\mathrm{v}}$

$$
C_{p}>C_{v}
$$

These are called molar heat capacities
i.e, $\quad C_{p}=\left(\frac{\partial H}{\partial T}\right)_{P}$
and

$$
C_{v}=\left(\frac{\partial \mathrm{U}}{\partial \mathrm{~T}}\right)_{\mathrm{V}}
$$

Note: For ideal gases, since $U$ and $H$ are only function of temperature, hence subscript $P$ and $V$ from $C_{p}$ and $C_{v}$
equation can be droped, which means $\mathrm{C}_{\mathrm{p}}=\left(\frac{\partial \mathrm{H}}{\partial \mathrm{T}}\right)_{\mathrm{P}}=\left(\frac{\partial \mathrm{H}}{\partial \mathrm{T}}\right)$ which means $\mathrm{C}_{\mathrm{p}}=\left(\frac{\partial \mathrm{H}}{\partial \mathrm{T}}\right)$
hence for any process involving ideal gas $\mathrm{dH}=\mathrm{C}_{\mathrm{p}} \mathrm{dT}$
similarily for change in internal energy involving ideal gas, the subscript V from the expression of $\mathrm{C}_{\mathrm{v}}$ can be dropped. Hence, $\mathrm{dU}=\mathrm{w} \mathrm{C}_{\mathrm{v}} \mathrm{dT}$ for all process involving ideal gases.
Hence $\Delta \mathrm{H}$ and $\Delta \mathrm{U}$ is equal to zero for isothermal process involving ideal gases.
Note : The relation $\mathrm{dH}=\mathrm{C}_{\mathrm{p}} \mathrm{dT}$ valid for any substance other than ideal gas only in isobaric process.
The relation $\mathrm{dU}=\mathrm{C}_{\mathrm{v}} \mathrm{dT}$ valid for any substance other than ideal gas only in isochoric process.

Ex. $10 \mathrm{dm}^{3}$ of $\mathrm{O}_{2}$ at $101.325 \mathrm{kP}_{\mathrm{a}}$ and 298 K is heated to 348 K . Calculate the heat absorbed, $\Delta \mathrm{H}$ and $\Delta \mathrm{U}$ of this process at
(a) at constant volume
(b) at constant volume

Given : $\mathrm{C}_{\mathrm{P}} / \mathrm{JK}^{-1} \mathrm{~mol}^{-1}=25.72+0.013(\mathrm{~T} / \mathrm{K})-3.86 \quad 10^{-6}(\mathrm{~T} / \mathrm{K})^{2}$
Assume ideal behaviour.
Sol. Amount of the gas, $n=\frac{\mathrm{PV}}{\mathrm{RT}}$
or $\quad \mathrm{n}=\frac{(101.325)(10)}{(8.314)(298)}=0.409 \mathrm{~mol}$.
(a) constant pressure

$$
\mathrm{q}_{\mathrm{P}}=\Delta \mathrm{H}=\mathrm{n} \int_{\mathrm{T}_{1}}^{\mathrm{T}_{2}} \mathrm{C}_{\mathrm{P}} \mathrm{dT}
$$

Here $\quad \mathrm{T}_{2}=348 \mathrm{~K}, \mathrm{~T}_{1}=298 \mathrm{~K}$
or $\quad q_{p}=0.409\left[(25.72)\left(T_{2}-T_{1}\right)+0.013\left(\frac{T_{2}^{2}}{2}-\frac{T_{1}^{2}}{2}\right)-\left(3.86 \times 10^{-6}\right)\left(\frac{\mathrm{T}_{2}^{3}}{3}-\frac{\mathrm{T}_{1}^{3}}{3}\right)\right]$
or $\quad q_{p}=0.409 \quad 1475.775=603.59 \mathrm{~J} \quad$ Ans.

$$
\begin{aligned}
\Delta \mathrm{U} & =\Delta \mathrm{H}-\Delta(\mathrm{PV}) \\
& =\Delta \mathrm{H}-\mathrm{P} \Delta \mathrm{~V}-\mathrm{V} \Delta \mathrm{P}
\end{aligned}
$$

at constant pressure

$$
\begin{aligned}
\Delta \mathrm{U} & =\Delta \mathrm{H}-\mathrm{P} \Delta \mathrm{~V}=\Delta \mathrm{H}-\mathrm{nR} \Delta \mathrm{~T} \\
& =603.59-0.4098 .314 \quad 50 \\
& =433.57 \mathrm{~J} \text { Ans. }
\end{aligned}
$$

(b) At constant volume

$$
\begin{aligned}
\mathrm{q}_{\mathrm{P}} & =\Delta \mathrm{H}=\int_{\mathrm{T}_{1}}^{\mathrm{T}_{2}} n C_{V} \mathrm{dT}=\int_{\mathrm{T}_{1}}^{\mathrm{T}_{2}} n C_{P} d T-\int_{T_{1}}^{\mathrm{T}_{2}} n R d T \\
& =603.59-170.02=433.57 \mathrm{~J} \quad \text { Ans. } \\
\Delta H & =\Delta \mathrm{U}+\Delta(\mathrm{PV})=\Delta \mathrm{U}+\mathrm{nR} \Delta \mathrm{~T}=603.59 \mathrm{~J} \quad \text { Ans. }
\end{aligned}
$$

Ex. Calculate the work done when 1 mol of zinc dissolves in hydrochloric acid at 273 K in :
(a) an open beaker
(b) a closed beaker at 300 K .

Sol. (a) From one mole of zinc, the no. of moles of $\mathrm{H}_{2}$ gas evolved $=1$
Hence volume of hydrogen gas evolved $=22.4$ litre (when $\mathrm{P}=1 \mathrm{~atm}$ and $\mathrm{T}=273 \mathrm{~K}$ )
$\therefore \mathrm{w}=-\mathrm{P} \Delta \mathrm{V}=-1 \quad 22.4$ litre atm

$$
=-22.4 \quad \frac{8.314}{0.082} \mathrm{~J}=-2271.14 \mathrm{~J} \quad \text { Ans. }
$$

(b) For a closed system $\mathrm{P}_{\text {ext }}=0$., therefore, $\mathrm{w}=0$.

Hence transfer of heat at constant volume brings about a change in the internal energy of the system whereas that at constant pressure brings about a change in the enthalpy of the system.
from the first law $\mathrm{dH}=\mathrm{dU}+\mathrm{d}(\mathrm{PV})$ for a differential change in state
if only ideal gas is involved $P V=n R T \quad d U=n_{v} d T \quad$ and $d H=n C_{p} d T$
substituting these results we get
$\mathrm{nC}_{\mathrm{p}} \mathrm{dT}=\mathrm{nC}_{\mathrm{v}} \mathrm{dT}+\mathrm{nRdT}$
$C_{p}=C_{v}+R$ valid only for ideal gas
relationship between $C_{p}$ and $C_{v}$ for real gases, liquid and solids is beyond the scope of JEE syllabus.
$\square$ Internal energy and enthalpy change in process involving ideal gases:
(i) Reversible isothermal process :

Take an ideal gas in a cylinder fitted with a frictionless piston. The cylinder is put in a large constant temperature bath and pressure over the piston is changed infinitesimally slowly.

If external pressure is decreased by infinitesimal small value, piston will go up by infinitesimal distance ' dx ' and temperature of gas inside piston decreases by dT (due to kinetic energy transfer of molecule to piston). To maintain thermal equilibrium infinitesimally small least dq will enter into the system. If the process is continued
for infinite steps, the path of process is an isotherm on P.V. graph.
If the gas is expanded from initial volume $V_{1}$ to final volume $V_{2}$ by gradually changing external pressure infinite steps, process is called reversible isothermal process.


Important points :
If the reversible isothermal expansion is reversed by gradually increasing the pressure the system will return to initial state retracing it's path. This mean path of reverssible process can be exactly reversed if conditions are reversed.

- Work done by the system during reversible isothermal expansion is maximum possible work obtainable from system under similar condition.
- Irreversible isothermal expansion : If external pressure over the piston is abruptly changed from the equilibrium value, the mechanical equilibrium of system is distured and piston rushes out :
This type of P.V. work is irreversible P.V. work. To calculate irreversible P.V. work law of conservation of energy is used. Suppose as a result of difference in pressure a piston moves out and aquire kinetic energy $\Delta \mathrm{K}$ and in the process volume increase by $\Delta \mathrm{V}$ then $\mathrm{w}_{\mathrm{irr}}=-\mathrm{P}_{\text {ext }} \Delta \mathrm{V}-\Delta \mathrm{K}$. If after sufficient times piston come back to equilibrium final state (off course in the process it moves up and down from equilibrium position
 many times), $\Delta \mathrm{K}=0$ : If all the aquired kinetic energy is transferred back to ideal gas,

$$
\mathrm{w}_{\mathrm{irr}}=-\mathrm{P}_{\text {ext. }} \Delta \mathrm{V}
$$

$\square \quad$ Many steps Irreversible isothermal expansion and compression (Comparison) consider an irrerversible expansion of an ideal gas from initial pressure of $P_{i}$ to final pressure of $P_{f}$ in four steps. The gas is allowed to expand against constant external pressure of $P_{1}, P_{2}, P_{3}$ and $P_{4}$ and finally $P_{f}$. Hence the system passes on to final state through four equilibrium states. The work done in the process is shown graphically. The area under the isotherm is the magnitude of reversible work. Clearly the magnitude of reversible work of expansion is greater than irreversible work. As the number of intermediate steps in


Volume $\rightarrow$ irrervisible expansion is incresesed, the magnitude of work increases, and as number of steps tend to infinity, $\mathrm{w}_{\text {irr }}$ tends to $\mathrm{w}_{\text {rev. }}$. The graphical comparison of irreversible and reversible work is shown in fig. Here, system is taken from initial state to the final state in four steps and isotherm represent magnitude of reversible work. Clearly, $\mathrm{w}_{\text {reversible }}$ is less than $\mathrm{w}_{\text {irreversible. }}$. Once again as the number of steps in irreversible compression increases, work required to compress the ideal gas decreases, and as number of steps tends to infinity, the $\mathrm{w}_{\text {rev }}=\mathrm{w}_{\text {irr }}$.
$\square$ Free expansion of ideal gas: When ideal gas is allowed to expand against zero external pressure, the process is called free expansion. $\mathrm{W}=0$ for free expansion. During the free expansion, the ideal gas do not lose any energy, and hence temperature of ideal gas remain constant. Hence, free expansion of ideal gas is an example of isothermal, adiabatic irreversible process.

However if a real gas is allowed to expand in vaccum, the gas may be cooled or heated up depending upon temperature of the real gas. The temperature above which a gas hots up upon expansion is called inversion temperature. The inversion temperature is strictly not in JEE sllaybus

Stoppered expansion(kind of an irreversible expansion): In this expansion, the gas is allowed to expand against constant external pressure but the piston is stopped at certain volume when system gradually attains equilibrium. In this type of expansion, the $P_{\text {external }}$ and $P_{\text {final }}$ are different. The stoppered expansion will help you realize that there can be infinite irreversible path's connection for any two given state at same temperature. ( the same can be said about reversible paths )
the work done during stoppered expansion can be given by

$$
w=-P_{e x t}\left(\frac{n R T_{f}}{P_{f}}-\frac{n R T_{i}}{P_{i}}\right) \quad \text { where } P_{\text {ext }} \text { and } P_{f} \text { are different }
$$

Reversible adiabatic process : In an adiabatic process, no loss or gain of heat takes place i.e., $d q=0$.
From first law, we have,

|  |  |
| :--- | :--- |
| Since | $d q=d U+d w$ |
| $\therefore$ | $d q$ |

For an ideal gas,
$\begin{array}{ll} & d U=C_{v} d T \\ \therefore & C_{v} d T=-d w=-p d V \\ \text { or, } & C_{v} d T=-(n R T / V) d V \\ \text { or, } & C_{v} d T / T+n R d V / V=0\end{array}$
Intergrating the above equation between $T_{1}$ and $T_{2}$ and $V_{1}$ and $V_{2}$, the initial and final temperature and volumes, we have,

$$
\begin{array}{ll}
\int_{\mathrm{T}_{1}}^{\mathrm{T}_{2}} \mathrm{C}_{\mathrm{v}} \frac{\partial \mathrm{~T}}{\mathrm{~T}}+\mathrm{nR} \int_{\mathrm{v}_{1}}^{\mathrm{v}_{2}} \frac{\partial \mathrm{~V}}{\mathrm{~V}}=0 \\
\text { or } & \mathrm{C}_{\mathrm{v}} \ln \frac{\mathrm{~T}_{2}}{\mathrm{~T}_{1}}+\mathrm{nR} \ln \frac{\mathrm{~V}_{2}}{\mathrm{~V}_{1}}=0
\end{array}
$$

Here $C_{v}$ is assumed to be independent of temperature.
But, $\quad C_{p}-C_{v}=n R$
Hence, from we get

$$
\mathrm{C}_{\mathrm{v}} \ln \frac{\mathrm{~T}_{2}}{\mathrm{~T}_{1}}+\left(\mathrm{C}_{\mathrm{p}}-\mathrm{C}_{\mathrm{v}}\right) \ln \frac{\mathrm{V}_{2}}{\mathrm{~V}_{1}}=0
$$

or, $\ln \frac{T_{2}}{T_{1}}=\frac{C_{p}-C_{v}}{C_{v}} \ln \frac{V_{1}}{V_{2}}$
we put,

$$
C_{p} / C_{v}=\gamma
$$

Equation may therefore be written as,

$$
\begin{aligned}
& \quad(\gamma-1) \ln \frac{\mathrm{V}_{2}}{\mathrm{~V}_{1}}+\ln \frac{\mathrm{T}_{2}}{\mathrm{~T}_{1}}=0 \\
& \text { or } \quad \frac{\mathrm{T}_{1}}{\mathrm{~T}_{2}}=\left(\frac{\mathrm{V}_{2}}{\mathrm{~V}_{1}}\right)^{\gamma-1} \\
& \text { or } \quad\left(\mathrm{T}_{1} \mathrm{~V}_{1}\right)^{\gamma-1}=\left(\mathrm{T}_{2} \mathrm{~V}_{2}\right)^{\gamma-1}=\text { constant }
\end{aligned}
$$

For an ideal gas,

$$
\begin{aligned}
& \frac{\mathrm{P}_{1} \mathrm{~V}_{1}}{\mathrm{~T}_{1}}=\frac{\mathrm{P}_{2} \mathrm{~V}_{2}}{\mathrm{~T}_{2}} \\
\text { or } & \frac{\mathrm{T}_{1}}{\mathrm{~T}_{2}}=\frac{\mathrm{P}_{1} \mathrm{~V}_{1}}{\mathrm{P}_{2} \mathrm{~V}_{2}}
\end{aligned}
$$

$\therefore$ from equation we have
$P_{1} V_{1}^{\gamma}=P_{2} V_{2}^{\gamma}=$ constant

In general, for a reversible adiabatic expansion

$$
\begin{aligned}
& \text { P. } \mathrm{V}^{\gamma}=\text { constant } \\
& \text { TV }^{\gamma-1}=\text { constant } \\
& \text { TP }^{1-\gamma / \gamma}=\text { constant }
\end{aligned}
$$


work done is given by either $\mathrm{w}=\mathrm{nC}_{\mathrm{v}}\left(\mathrm{T}_{2}-\mathrm{T}_{1}\right)$ or rearranging it gives $\mathrm{w}=\left(\mathrm{P}_{2} \mathrm{~V}_{2}-\mathrm{P}_{1} \mathrm{~V}_{1}\right) / \gamma-1$
For an isothermal expansion, $\mathrm{PV}=$ constant.but for an reversible adiabatic expansion $\mathrm{PV}^{\gamma}=$ constant differentiating both $P V$ and $P V^{\gamma-1}$ with respect to $V$ we get for isothermal process $d P / d V=-P / V$ while for adiabatic process $\mathrm{dP} / \mathrm{dV}=-\gamma(\mathrm{P} / \mathrm{V})$ since $\gamma$ is always $>1$ slope of $\mathrm{P} V$ curve is more negative in case of adiabatic process.

In figure, pressure and volume are plotted for isothermal and adiabatic cases. It is evident that a given pressure fall produces a lesser volume increase in the adiabatic case, because the temperature also falls during the adiabatic expansion.
$\square$ The irreversible adiabatic process : Suppose an ideal gas is confined in a adiabatic container fitted with friction less piston. If the thermodynamic equilibrium of system is disturbed by changing external pressure suddenly by finite value and let the system come to equilibrium the process is irreversible adiabatic process. The work done (w) is given by

$$
\begin{aligned}
& \Delta U=w=-P_{\text {ext }}\left(V_{f}-V_{i}\right) \\
& \Delta U=n C_{v}\left(T_{f}-T_{i}\right) \\
& \Rightarrow \quad n C_{v}\left(T_{f}-T_{i}\right)=-P_{\text {ext }}\left(V_{f}-V_{i}\right) \\
& n C_{v}\left(T_{f}-T_{i}\right)=-P_{\text {ext }}\left(\frac{n R T_{f}}{P_{f}}-\frac{n R T_{i}}{P_{i}}\right)
\end{aligned}
$$

solving this equation for $T_{f}$
now $w=\Delta U=n C_{v}\left(T_{2}-T_{1}\right)$

$$
\mathrm{w}=\left[\frac{\mathrm{P}_{\mathrm{f}} \mathrm{~V}_{\mathrm{f}}-\mathrm{P}_{\mathrm{i}} \mathrm{~V}_{\mathrm{i}}}{\gamma-1}\right]
$$

Comparison of isothermal and adiabatic process :
Starting from same state, if system is allowed to expand to same final pressure,
$\left|w_{\text {rev, isothermal }}\right|>\left|w_{\text {rev,adiabatic }}\right|$.
In reversible isothermal process, heat is entering from surrounding, while in adiabatic process, work is done on the expansion of internal energy of system.

Starting from same initial state, if system is compressed to same final pressure, $\mathrm{w}_{\text {rev,adia }}>\mathrm{w}_{\text {rev,iso }}$. During adiabatic compression, the work done is getting stored in the system, and temperature of system increses, the gas become less and less compressible, and greater work is required to compress the system.
$\square \quad$ Change in internal energy and enthalpy in chemical reactions : Enthalpy and internal energy change in chemical reaction involve change in potential energy due to chemical change. During chemical change transformation of bonds take place. If the bonds in product are more stable, leading to decrease in potential energy of atom and molecules, the enthalpy and internal energies decreases. In the process surplus energy is librated and process is called exothermic process.
During endothermic chemical process which take place absorbing energy from surrounding, the potential energy of system of chemical substance increases.
Consider a chemical reaction

$$
a A+b B--->c C+d D
$$

The internal energy change can be given as (Theoratically)
$\Delta U=c U_{c}+d U_{d}-a U_{a}-b U_{b}$
where $U_{a}, U_{b}, U_{c}, U_{d}$ etc. are molar internal enegy of respective species.
since absolute internal energies cannot be determine, $U_{i}$ are determined with respect to internal energy of elements in their most stable state. The internal energies of elements in their most stable allotropic modification is arbitary taken as zero at 298 K and 1 atm pressure.
also, $\Delta_{\mathrm{r}} \mathrm{U}=\mathrm{q}_{\mathrm{v}}$ for reaction taking place under constant volume and temperature condition. For the similar reaction occuring at constant pressure and temperature, enthalpy change, $\Delta \mathrm{H}$ is given by
$\Delta \mathrm{H}=\mathrm{cH}_{\mathrm{c}}+\mathrm{dH}_{\mathrm{d}}-\mathrm{aH}-\mathrm{bH}_{\mathrm{b}}$
where $H$ are enthalpies of respective species
however $\Delta \mathrm{H}$ is equal to heat exchange during chemical process at constant pressure and temperature.

$$
\Delta_{\mathrm{r}} \mathrm{H}=\mathrm{q}_{\mathrm{p}} \quad \text { for reaction taking place under constant pressure and temperature conditions }
$$

Relationship between $\Delta_{\mathrm{r}} \mathrm{H}$ and $\Delta_{\mathrm{r}} \mathrm{U}$ in chemical reactions : For a general chemical reaction given by $\mathrm{aA}+\mathrm{bB}--->\mathrm{cC}+\mathrm{dD}$
$\Delta_{\mathrm{r}} \mathrm{H}=\mathrm{cH}_{\mathrm{c}}+\mathrm{dH}_{\mathrm{d}}-\mathrm{aH}-\mathrm{aH}_{\mathrm{b}}$ but $\mathrm{H}_{\mathrm{i}}=\mathrm{U}_{\mathrm{i}}+\mathrm{PV} \mathrm{V}_{\mathrm{i}}$
substituting the value of molar enthalpies of substance in equation (1) we get

$$
\begin{align*}
& \Delta_{\mathrm{r}} \mathrm{H}=\mathrm{c} \mathrm{U}_{\mathrm{c}}+\mathrm{d} \mathrm{U}_{\mathrm{d}}-\mathrm{aU} \mathrm{U}_{\mathrm{a}}-\mathrm{b} \mathrm{U}_{\mathrm{b}}+\mathrm{P}\left(\mathrm{cV}_{\mathrm{c}}+\mathrm{dV} \mathrm{~d}_{\mathrm{d}}-\mathrm{aV}_{\mathrm{a}}-\mathrm{bV} \mathrm{~b}_{\mathrm{b}}\right) \\
& \Delta_{\mathrm{r}} \mathrm{H}=\Delta_{\mathrm{r}} \mathrm{U}+\mathrm{P}\left(\mathrm{~V}_{\mathrm{f}}-\mathrm{V}_{\mathrm{i}}\right) \quad \ldots \ldots \ldots \ldots \ldots \text { (2) } \tag{2}
\end{align*}
$$

(a) If all the reactant and products are ideal gases $V_{c}, V_{d}, V_{a}$ and $V_{b}$ all are equal to molar volume of ideal gas e.g. $\mathrm{V}=\mathrm{RT} / \mathrm{P}$ which on substitution in previous equation gives

$$
\begin{align*}
\Delta_{\mathrm{r}} \mathrm{H} & =\Delta_{\mathrm{r}} \mathrm{U}+(\mathrm{d}+\mathrm{c}-\mathrm{a}-\mathrm{b}) \mathrm{RT} \\
\Delta_{\mathrm{r}} \mathrm{H} & =\Delta_{\mathrm{r}} \mathrm{U}+\Delta_{\mathrm{n}_{\mathrm{g}}} \mathrm{RT} \ldots \ldots \ldots \ldots \ldots \ldots \tag{3}
\end{align*}
$$

Where $\Delta n_{g}$ is difference of stoichiometric cofficient of gaseous products and gaseous reactants.
(b) In case of liquid and solids present in chemical equations, their molar volumes can be ignored in comparison to molar volume of ideal gases and hence do not count stoichiometric cofficient of solid and liquids in $\Delta \mathrm{n}_{\mathrm{g}}$.
(c) In case of non ideal behaviour of gases, equation (2) should be used.

Change in internal energy and enthalpy in phase transition : At certain temperature under one atmospheric pressure, one phase changes into other phase by taking certain amount of Heat. The temperatrue at which this happens is called transition temperature and heat absorbed druing the process is called Enthalpy of phase transition. Heat absorbed during transition is exchanged at constant pressure and temperatrue and it is significant to know that the process is reversible.
Fusion : Solid ice at 273 K and 1 atm pressure reversibly changes into liquid water. Reversibly, isothermally and isobarically, absorbing heat know as latent heat of fusion.or enthalpy of fusion.
Vaporisation : Water at 373 K and 1 atm pressure changes into its vapors absorbing heat known as latent heat of vaporisation. The latent heat of vaporisation is heat exchanged isothermally, isobarically and reversibly to convert water into its vapour at boiling point.

Internal energy change of phase transitions involving gas phase has no practical significance because it is not possible to carry out $\Delta \mathrm{U}$ of phase transition directly through an experiment. However $\Delta \mathrm{U}$ of phase transition can be determined theoretically from experimentally obtained value of $\Delta \mathrm{H}$ of phase transition.

$$
\begin{aligned}
& \mathrm{H}_{2} \mathrm{O}(\ell) \quad \longrightarrow \mathrm{H}_{2} \mathrm{O}(\mathrm{~g}) \\
& \Delta \mathrm{H}_{\text {vaporisation }}=\Delta \mathrm{U}_{\text {vaporisation }}+\mathrm{P}\left(\mathrm{~V}_{\mathrm{f}}-\mathrm{V}_{\mathrm{i}}\right) \\
& \Delta \mathrm{H}_{\text {vaporisation }}=\Delta \mathrm{U}_{\text {vaporisation }}+\{\mathrm{RT} / \mathrm{V}\}\left\{\mathrm{Vg}_{\mathrm{g}}\right\}
\end{aligned}
$$

ignoring volume of liquid as compared to molar volume of gas

$$
\Rightarrow \quad \Delta \mathrm{H}_{\text {vap. }}=\Delta \mathrm{U}_{\text {vap. }}+\mathrm{RT}
$$

where R is gas constant and T absolute temperature for condensed phase transitions like solid liquid transitions

$$
\Delta \mathrm{H}_{\text {vap. }} \sim \Delta \mathrm{U}_{\text {vap. }}
$$

- Variation of enthalpy with temperature (KIRCHHOFF'S EQUATION): The enthalpy of chemical reactions and phase transition do vary with temperature. Although the variation in $\Delta \mathrm{H}$ with temprature is usually small compared to the value of $\Delta \mathrm{H}$ itself,

- Since H is state function : Change in enthalpy in cyclic process is equal to zero. To calculate enthalpy change $\left(\Delta \mathrm{H}_{2}\right)$ at temperataure $\mathrm{T}_{2}$ at constant pressure consider cyclic process shown in figure. It is clear
$\Delta H_{3}=$ change in enthalpy of $A$ when temperature is raised from $T_{1}$ to $T_{2}$ at constant pressure. $\Delta H_{3}=\int_{T_{1}}^{T_{2}} C_{p, B} d T$
$\Delta H_{4}=$ Change in enthalpy taking 1 mole of $B$ at constant pressure from $T_{1}$ to $T_{2}=\Delta H_{4}=\int_{T_{2}}^{T_{1}} C_{p, A} d T$
now : $\Delta \mathrm{H}_{3}+\Delta \mathrm{H}_{1}+\Delta \mathrm{H}_{4}=\Delta \mathrm{H}_{2}$
$\Rightarrow \Delta \mathrm{H}_{2}-\Delta \mathrm{H}_{1}=\Delta \mathrm{H}_{3}+\Delta \mathrm{H}_{4}$
$\Rightarrow \Delta \mathrm{H}_{2}-\Delta \mathrm{H}_{1}=\int_{\mathrm{T}_{1}}^{\mathrm{T}_{2}}\left(\mathrm{C}_{\mathrm{p}, \mathrm{B}}-\mathrm{C}_{\mathrm{p}, \mathrm{A}}\right) \mathrm{dT}$
$\Rightarrow \Delta \mathrm{H}_{2}-\Delta \mathrm{H}_{1}=\Delta_{\mathrm{r}} \mathrm{C}_{\mathrm{p}}\left(\mathrm{T}_{2}-\mathrm{T}_{1}\right)$ If $\Delta_{\mathrm{r}} \mathrm{C}_{\mathrm{p}}$ is independent of 'temperature'
Second law : There are two types of processes reversible process or quasi static process in which system remains in equilibrium with surrounding through out the process.
However reversible processes can not take place on it's own - and are not natural process. Reversible process do not lead to production of disorder.
On the other hand most of the processes taking place around us is example of irreversible process. Irreversible process also natural processes or spontaneous processes.
Example of natural processes :
(i) Water flowing down hill
(ii) Heat flowing from hot body towards cold body on it's own
(iii) mixing of two gases.
(iv) Rusting of iron
(v) Evaporation of water at room temperature.
(vi) Formation of $\mathrm{NH}_{3}(\mathrm{~g})$ from $\mathrm{N}_{2}(\mathrm{~g})$ and $\mathrm{H}_{2}(\mathrm{~g})$ gas in a closed container.
(vii) Expansion of ideal gas in vacuum
(viii) Burning of coal in $\mathrm{O}_{2}$

Every natural process leads to production of disorder. (During irreversible process system moves from ordered state to disordered state).
The second law of thermodynamics :
The second law of thermodynamics predict's direction of natural change. It do so with the help of state function 'S' - called entropy of system. But for predicting direction of natural change another quantity $\mathrm{S}_{\text {surrounding }}$ is also needed. $\mathrm{S}_{\text {surrounding }}$ which is called entropy of surrounding is a path dependent quantity.

$$
\begin{aligned}
& \mathrm{dS}_{\text {system }}=\frac{\mathrm{dq}_{\mathrm{rev}}}{\mathrm{~T}} \\
& \mathrm{dS}_{\text {surr }}=-\frac{\mathrm{dq}}{\mathrm{~T}}
\end{aligned}
$$

Since $\mathrm{S}_{\text {system }}$ is state function - If a system make transition from state A to state B - by infinite paths in few of them may be reversible and other may be irreversible. $\Delta \mathrm{S}_{\mathrm{AB}}$ will be same irrespective of path (A direct consequence of $\mathrm{S}_{\text {system }}$ being a state function).

However, If same transition from $A$ to $B$ is done by different irreversible path's, $\Delta \mathrm{S}_{\text {surrounding }}$ will be different in all processes. However if transition from $A \rightarrow B$ take place by many reversible path's, $\Delta \mathrm{S}_{\text {surr }}$ along each path will be same because

$$
\begin{aligned}
& -\sum_{A \rightarrow B}^{\text {path } 1} \frac{\mathrm{dq}_{\text {rev }}}{T}=-\Delta S_{\text {system }}=-\sum_{A \rightarrow B}^{\text {path } 2} \frac{\mathrm{dq}_{\text {rev }}}{T} \\
& \Rightarrow \quad \underset{A \rightarrow B}{\Delta S_{\text {surr }}} \text { (path 1) }=-\Delta \underset{A \rightarrow B}{\Delta S_{\text {system }}}=-\underset{A \rightarrow B}{\Delta S_{\text {surr }}} \text { (path 2) }
\end{aligned}
$$

## Entropy change of system and surrounding in reversible and irrversible process

Note that $\Delta \mathrm{S}_{\text {surr }}=-\frac{\mathrm{q}_{\text {actual }}}{\mathrm{T}}$
The central concept of entropy is given briefly, because JEE syllabus deals with consequence of second law rather than it's derivation.
Prediction of spontaneity of process : If total entropy change in a process is positive the process must be spontaneous.

$$
\Delta \mathrm{S}_{\text {system }}+\Delta \mathrm{S}_{\text {surrounding }}>0 \text { for spontaneous change. }
$$

The second law of thermodynamics was developed during course of development of cyclic engines. Second law was discovered while studying efficiency of steam engines. In 1824 a french engineer Sodi carnot pointed out that for a cyclic heat engine to produce continuous mechanical works, it must exchange heat with two bodies at different temperature without a cold body to discard heat, the engine can-not function continuously.

- Entropy change in isolated system (isolated system = sys + surr)

Consider a system taken from state A to state B by an irreversible path and returned to state A by a reversible path. Since one of the step is irreversible, according to Clasius inequality, sum of $\mathrm{q} / \mathrm{T}$ over the cycle must be less than zero. Hence


$$
\sum_{A \rightarrow B} \frac{q_{i r r}}{T}+\sum_{B \rightarrow A} \frac{q_{\text {rev }}}{T} \leq 0 \Rightarrow \sum_{A \rightarrow B} \frac{q_{i r r}}{T}=-\sum_{B \rightarrow A} \frac{q_{\text {rev }}}{T}
$$

But $-\sum_{\mathrm{B} \rightarrow \mathrm{A}} \frac{\mathrm{q}_{\mathrm{rev}}}{\mathrm{T}}=\sum_{\mathrm{A} \rightarrow \mathrm{B}} \frac{\mathrm{q}_{\mathrm{rev}}}{\mathrm{T}}$ since the process is reversible
for infinitesimally small change

$$
\begin{array}{ll} 
& \left(\frac{\left(\frac{d q}{T}\right)_{A \rightarrow B}=d S_{\text {system } A \rightarrow B}}{}\right. \\
\Rightarrow & \mathrm{dS}_{\text {system }}-\left(\frac{d q}{T}\right)_{A \rightarrow B}>0 \\
\Rightarrow & \mathrm{dS}_{\text {system } A \rightarrow B}+\mathrm{dS}_{\text {sur } A \rightarrow B}>0 \\
\Rightarrow & \Delta \mathrm{~S}_{\text {Total isolated sys }}>0
\end{array}
$$

- Entropy calculation in process involving ideal gases.

From First law

$$
\begin{array}{r}
\mathrm{dq}=\mathrm{dU}+\mathrm{PdV} \\
\Rightarrow \quad \frac{\mathrm{dq}_{\mathrm{rev}}}{\mathrm{~T}}=\frac{\mathrm{dU}}{\mathrm{~T}}+\frac{\mathrm{PdV}}{\mathrm{~T}}
\end{array}
$$

But for ideal gas

$$
\begin{array}{rlr} 
& \frac{d U}{T}=\frac{n C_{v} d T}{T} & \left\{\because d U={ }_{n} C_{v} d T\right\} \\
\Rightarrow \quad & \mathrm{dS}_{\text {sys }} & =\frac{n C_{v} d T}{T}+\frac{n R}{V} d V
\end{array}
$$

Integration gives

$$
\Delta \mathrm{S}=\mathrm{nC}_{\mathrm{V}} \ln \frac{\mathrm{~T}_{2}}{\mathrm{~T}_{1}}+\mathrm{nR} \ln \left(\frac{\mathrm{~V}_{2}}{\mathrm{~V}_{1}}\right)
$$

For isothermal process

$$
\Delta \mathrm{S}=\mathrm{nR} \ln \frac{\mathrm{~V}_{2}}{\mathrm{~V}_{1}}
$$

For isochoric process

$$
\Delta \mathrm{S}=\mathrm{nC}_{\mathrm{V}} \ln \frac{\mathrm{~T}_{2}}{\mathrm{~T}_{1}}
$$

For isobaric process

$$
\Delta \mathrm{S}=\mathrm{nC}_{\mathrm{p}} \ln \frac{\mathrm{~T}_{2}}{\mathrm{~T}_{1}}
$$

## - Entropy change in chemical Reaction :

From application of third law absolute entropy of every compound or element can be deduced for a general chemical reaction taking place at given condition

$$
\begin{aligned}
& a \mathrm{~A}+\mathrm{bB}---\mathrm{cC}+\mathrm{dD} \\
& \Delta \mathrm{~S}=\Delta \mathrm{S}_{\text {system }}=\text { entropy change of reaction } \\
\Rightarrow \quad & =\left(\mathrm{aS}_{\mathrm{C}}+\mathrm{dS}_{\mathrm{D}}-\mathrm{aS}_{\mathrm{A}}-\mathrm{bS}_{\mathrm{B}}\right)
\end{aligned}
$$

where $S_{C}, S_{D}, S_{A}$ and $S_{B}$ are molar entropy of substance $A, B, C$ and $D$ under given circumtance.

- Entropy change in phase transition :

Fusion :
When solid ice is heated below 273 K at external pressure of 1 atm it's temperature slowly rises. At 273 K however. its start melting into liquid without increase in temperature. The process is reversible phase transition from solid to liquid represented as :

$$
\mathrm{H}_{2} \mathrm{O}(\mathrm{~s}) \rightleftharpoons \mathrm{H}_{2} \mathrm{O}(\ell)
$$

Since process is reversible (you can safely assume that phase transition at constant temperature and pressure are reversible phase transitions).

Now $\Delta \mathrm{S}_{\text {Total }}=0 \quad$ (since process is reversible)
$\Delta \mathrm{S}_{\text {system }}+\Delta \mathrm{S}_{\text {surr }}=0$
also $\quad \Delta \mathrm{S}_{\text {surrounding }}=\frac{-\Delta \mathrm{H}_{\text {fusion }}}{\mathrm{T}_{\mathrm{f}}}$ (here $\mathrm{T}_{\mathrm{f}}=$ freezing point)
$\Rightarrow \quad \Delta \mathrm{S}_{\text {Total }}=\frac{\Delta \mathrm{H}_{\text {fusion }}}{\mathrm{T}_{\mathrm{f}}}=0$
$\Rightarrow \quad \Delta \mathrm{S}_{\text {fustion }}=\frac{\Delta \mathrm{H}_{\text {fusion }}}{\mathrm{T}_{\mathrm{f}}}$ entropy of fusion at Melting point.
Vapourisation : From you day to day experience you know that under atmospheric pressure temperature of $\mathrm{H}_{2} \mathrm{O}(\ell)$ can not exceed 373 K . Since at 373 K liquid $\mathrm{H}_{2} \mathrm{O}$ undergo phase transition.

$$
\mathrm{H}_{2} \mathrm{O}(\ell) \rightleftharpoons \mathrm{H}_{2} \mathrm{O}(\mathrm{~g})
$$

$$
\text { since } \Delta \mathrm{S}_{\text {Total }}=0 \quad \text { (Process is reversible) }
$$

$$
\Delta \mathrm{S}_{\text {system }}+\Delta \mathrm{S}_{\text {surr }}=0
$$

$$
\Delta \mathrm{S}_{\text {system }}=\Delta \mathrm{S}_{\text {fusion }}=\mathrm{S}_{\mathrm{H}_{2} \mathrm{O}(\mathrm{~g})}-\mathrm{S}_{\mathrm{H}_{2} \mathrm{O}(\ell)}
$$

$$
\Delta \mathrm{S}_{\text {surrounding }}=-\frac{\Delta \mathrm{H}_{\text {vap }}}{\mathrm{T}_{\mathrm{b}}} \text { (here } \mathrm{T}_{\mathrm{b}}=\text { melting point) }
$$

Note : Boiling point at 1 atm pressure is called normal boiling point. There can be infinite boiling points of liquid depending upon external pressure we applying on boiling vessel.
$\square$ Entropy and criteria of spontanity of chemical process :
The entropy change of chemical reaction together with entropy change of surrounding determine spontanity of a chemical process under given set of condition.
$\Delta \mathrm{S}_{\text {Total }}=\Delta_{\mathrm{r}} \mathrm{S}-\frac{\Delta_{\mathrm{r}} \mathrm{H}}{\mathrm{T}}$
If $\Delta_{\mathrm{r}} \mathrm{S}=$ positive and very large while $\Delta_{\mathrm{r}} \mathrm{H}$ is negative and large this means $\Delta \mathrm{S}_{\text {Total }}>0$.
If $\Delta_{\mathrm{r}} \mathrm{S}=$ positive but small and $\Delta_{\mathrm{r}} \mathrm{H}$ is negative but having large value.
$\Rightarrow \quad$ If $\Delta \mathrm{S}_{\text {Total }}$ is +ive due to large +ive value of $\Delta_{\mathrm{r}} \mathrm{S}$, we can say reaction is entropy driven that is increased in disorder in forward direction is the driving force of reaction which takes it in forward direction. $\left(\mathrm{H}_{2} \mathrm{O}(\ell) \longrightarrow \mathrm{H}_{2} \mathrm{O}(\mathrm{g})\right.$ above 373 K at 1 atm)
$\Rightarrow \quad$ Sometimes reaction go completely in forward direction inspite of negative entropy change in reaction due to large -ive value of $\Delta_{\mathrm{r}} \mathrm{H}$. These reaction are enthalpy driven.

Example : $\quad \mathrm{C}_{2} \mathrm{H}_{2}(\mathrm{~g})+\frac{5}{2} \mathrm{O}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{CO}_{2}(\mathrm{~g})+\mathrm{H}_{2} \mathrm{O}(\ell)$
Spontaneous and non Spontaneous

| $\begin{gathered} \hline \text { Sign of } \\ \Delta H \\ \hline \end{gathered}$ | Sign of $\Delta \mathrm{S}$ | Comment | Example | $\Delta \mathrm{H}_{298}$ | $\Delta \mathrm{S}_{298}$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| - | + | spontaneous | $\mathrm{H}_{2}(\mathrm{~g})+\mathrm{Cl}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{HCl}(\mathrm{g})$ | -185 | 14.1 |
|  |  | at all temperature | $\mathrm{C}(\mathrm{s})+\mathrm{O}_{2}(\mathrm{~g}) \longrightarrow \mathrm{CO}_{2}(\mathrm{~g})$ | -394 | 3 |
| - | - | spontaneous | $\mathrm{H}_{2}(\mathrm{~g})+1 / 2 \mathrm{O}_{2} \longrightarrow \mathrm{H}_{2} \mathrm{O}(\ell)$ | -44 | -119 |
|  |  | at low temperature | $2 \mathrm{SO}_{2}(\mathrm{~g})+\mathrm{O}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{SO}_{3}(\mathrm{~g})$ | -198 | -187 |
| + | + | spontaneous | $\mathrm{NH}_{4} \mathrm{Cl}(\mathrm{s}) \longrightarrow \mathrm{NH}_{3}(\mathrm{~g})+\mathrm{HCl}(\mathrm{g})$ | 176 | 284 |
|  |  | at high temperature | $\mathrm{N}_{2}(\mathrm{~g})+\mathrm{O}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{NO}(\mathrm{g})$ | 180 | 25 |
| + | - | non spontaneous | $3 \mathrm{O}_{2} \longrightarrow 2 \mathrm{O}_{3}$ | 286 | -137 |
|  |  | at all temperature | $2 \mathrm{H}_{2} \mathrm{O}(\ell)+\mathrm{O}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{H}_{2} \mathrm{O}_{2}(\ell)$ | 196 | -126 |

Ex. Will $\Delta \mathrm{S}$ be positive or negative in the following processes ? Discuss qualitatively
(a) $\mathrm{H}_{2} \mathrm{O}(\mathrm{s}) \longrightarrow \mathrm{H}_{2} \mathrm{O}(\ell)$
(b) $\mathrm{H}_{2} \mathrm{O}(\ell) \longrightarrow \mathrm{H}_{2} \mathrm{O}(\mathrm{g})$
(c) $\mathrm{H}_{2}(\mathrm{~g})+\mathrm{Cl}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{HCl}(\mathrm{g})$
(d) $\frac{1}{2} \mathrm{~N}_{2}(\mathrm{~g})+\frac{3}{2} \mathrm{H}_{2}(\mathrm{~g}) \longrightarrow \mathrm{NH}_{3}(\mathrm{~g})$
(e) $2 \mathrm{H}_{2}(\mathrm{~g})+\mathrm{N}_{2}(\mathrm{~g}) \longrightarrow \mathrm{N}_{2} \mathrm{H}_{4}(\ell)$
(f) $\mathrm{Cl}_{2}(\mathrm{~g}) \longrightarrow 2 \mathrm{Cl}(\mathrm{g})$

Sol. As we have discussed that the entropy of reaction is more if there is a change in value of $\Delta \nu_{\mathrm{g}}$ (the change in the stoichiometric number of gaseous species), since the entropy of gases is much larger than the entropy of the condensed phases.
$\therefore$ for process $\quad$ (a) $\Delta \mathrm{S}$ is +ve

| for process | (b) $\Delta \mathrm{S}$ is +ve |
| :--- | :--- |
| for process | (c) $\Delta \mathrm{S}$ is zero |
| for process | (d) $\Delta \mathrm{S}$ is negative |
| for process | (e) $\Delta \mathrm{S}$ is negative |
| for process | (f) $\Delta S$ is positive |

Ex. Sulphur exists in more than one solid form. The stable form. The stable form at room temperatrure is rhombic sulphur. But above room temperature the following reaction occurs :

$$
\mathrm{s} \text { (rhombic) } \longrightarrow \mathrm{s} \text { (mono clinic) }
$$

Thermodynamic measurements reveal that at $101.325 \mathrm{kP}_{\mathrm{a}}$ and 298 K ,

$$
\Delta_{\mathrm{r}} \mathrm{H}=276.144 \mathrm{~J} \mathrm{~mol}^{-1} \text { and } \Delta_{\mathrm{r}} \mathrm{G}=75.312 \mathrm{~J} \mathrm{~mol}^{-1}
$$

(a) Compute $\Delta_{\mathrm{r}} \mathrm{s}$ at 298 K
(b) Assume that $\Delta_{r} \mathrm{H}$ and $\Delta_{\mathrm{r}} \mathrm{s}$ do not vary significantly with temperature, compute $\mathrm{T}_{\text {eq }}$, the temperature at which rhombic and monoclinic sulphur exist in equilibrium with each other.

Sol. (a) Since

$$
\Delta_{\mathrm{r}} \mathrm{G}=\Delta_{\mathrm{r}} \mathrm{H}-\mathrm{T} \Delta_{\mathrm{r}} \mathrm{~S},
$$

Therefore

$$
\begin{aligned}
& \Delta_{\mathrm{r}} \mathrm{~S}=\frac{\Delta_{\mathrm{r}} \mathrm{H}-\Delta_{\mathrm{r}} \mathrm{G}}{\mathrm{~T}}=\frac{276.144 \mathrm{~J} \mathrm{~mol}^{-1}-75.312 \mathrm{~J} \mathrm{~mol}^{-1}}{298 \mathrm{~K}} \\
& =0.674 \mathrm{~J} \mathrm{~K}^{-1} \mathrm{~mol}^{-1}
\end{aligned}
$$

(b) When the rhombic sulphur is in equilibrium with monoclinic sulphur, we would have

$$
\Delta_{\mathrm{r}} \mathrm{G}=0=\Delta_{\mathrm{r}} \mathrm{H}-\mathrm{T}_{\mathrm{eq}} \Delta_{\mathrm{r}} \mathrm{~S}
$$

Thus $\quad \mathrm{T}_{\text {eq }}=\frac{\Delta_{\mathrm{r}} \mathrm{H}}{\Delta_{\mathrm{r}} \mathrm{S}}=\frac{276.144 \mathrm{~J} \mathrm{~mol}^{-1}}{0.674 \mathrm{~J} \mathrm{~mol}^{-1}}$

$$
=409.7 \mathrm{~K}
$$

Ex. At 1 atm and 27 C , will the vaporisation of liquid water be spontaneous ? Given $\Delta \mathrm{H}=9710 \mathrm{cal}$ and $\Delta \mathrm{s}=26 \mathrm{eu}$.

Sol. $\mathrm{H}_{2} \mathrm{O}(\ell)=\mathrm{H}_{2} \mathrm{O}(\mathrm{g}) \quad(\mathrm{P}=1 \mathrm{~atm})$

$$
\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{~S}=9710-26 \quad 300=+1910 \mathrm{cal}
$$

since $\Delta \mathrm{G}$ is positive, at 1 atm , vaporisation is not possible. Rather the reverse process of condensation will occur. The temperature at which the liquid and vapour will be equiv. can be obtained, by putting $\Delta \mathrm{G}=0$, i.e

$$
\begin{aligned}
& \Delta \mathrm{G}=9710-26 \mathrm{~T}=0 \\
& \mathrm{~T}=373.4 \mathrm{C}
\end{aligned}
$$

This indeed is the boiling point of water at 1 atm.
Ex.

| Gases | $\Delta \mathrm{G}_{\mathrm{f}}(\mathrm{Cal} / \mathrm{mole})$ |
| :---: | :---: |
| CO | -32.80 |
| $\mathrm{H}_{2} \mathrm{O}$ | -54.69 |
| $\mathrm{CO}_{2}$ | -94.26 |
| $\mathrm{H}_{2}$ | 0 |

Estimate the standard free energy change in the chemical reaction

$$
\mathrm{CO}+\mathrm{H}_{2} \mathrm{O}=\mathrm{CO}_{2}+\mathrm{H}_{2}
$$

Sol. Using the necessary data from the table

\[

\]

Third law of thermodynamics :
Third law of thermodynamics helps in determining absolute entropy of substances. It is based on an assumption that entropy of every perfectly crystalline substance is zero at zero
Kelvin. This is justified because, at absolute zero every substance is in state of lowest energy and position of every atom or molecule is defined in solid. Hence at $T=0 \quad S(T=0)=0 \quad$ Third law If we have sufficient heat capacity data (and the data on phase changes) we could write

$$
\begin{equation*}
S(T)=S(T=0)+\int_{0}^{r} \frac{C_{p}}{T} d T \tag{i}
\end{equation*}
$$

(If there is a phase change between 0 K and T , we would have to add the entropy of the phase change.) If $C_{p}$ were constant near $T=0$, we would have,

$$
S(T)=S(T=0)+C_{p} \ln \frac{T}{0}
$$

Which is undefined. Fortunately, experimentally $C_{p} \rightarrow 0$ as $T \rightarrow 0$. For nonmetals $C_{p}$ is proportional to $T^{3}$ at low temperature. For metals $C_{p}$ is proportional to $T^{3}$ at low temperatures but shifts over to being proportional to T at extermely low temperatures. (The latter happens when the atomic motion "freezes out" and the heat capacity is due to the motion of the conduction electrons in the metal.)
equation (i) could be used to calculate absolute entropies for substances if we know what the entropy is at absolute zero. Experimentally it appears that the entropy at absolute zero is the same for all substances. The third law of thermodynamics modifies this observation and sets

$$
S(T=0)=0
$$

for all elements and compounds in their most stable and perfect crystalline state at absolute zero and one atmosphere pressure. (All except for helium, which is a liquid at the lowest observable temperatures at one atmosphere.)

The advantage of this law is that it allows us to use experimental data to compute the absolute entropy of a substance. For example, suppose we want to calculate the absolute entropy of liquid water at 25 C . We would need to known the $C_{p}$ of ice from 0 K to 273.15 K . We also need the heat of fusion of water at its normal melting point. With all of this data, which can be obtained partly from theory and partly from experiment, we find

$$
\mathrm{S}_{\mathrm{H}_{2} \mathrm{O}}(25 \mathrm{C})=0+\int_{0}^{273.15} \frac{\mathrm{C}_{\mathrm{p}}(\mathrm{~s})}{\mathrm{T}} \mathrm{dT}+\frac{\Delta \mathrm{H}_{\mathrm{fus}}}{273.15}+\int_{273.15}^{298.15} \frac{\mathrm{C}_{\mathrm{p}}(\mathrm{l})}{\mathrm{T}} \mathrm{dT} .
$$

Some substances may undergo several phase changes.

## $\square$ Gibb's function :

Entropy is a universal criteria of spontaneity. This means for any process if $\Delta \mathrm{S}_{\text {Total }}>0$ the process is spontaneous. Most of the chemical process take place at constant temperature and pressure. A very useful criteria of spontaneity of process at constant temperature and pressure is Gibb's function :

Gibb's function (G) is defined as

$$
\begin{equation*}
G=H-T S \tag{i}
\end{equation*}
$$

Gibb's function and spontaneous process :
from $2^{\text {nd }}$ law we known :

$$
\begin{equation*}
\frac{\mathrm{dq}}{\mathrm{~T}} \leq \mathrm{dS}_{\text {system }}: \text { Less than sign for if } \mathrm{q}=\mathrm{q}_{\mathrm{irr}} \tag{ii}
\end{equation*}
$$

$\Rightarrow \quad \mathrm{dq} \leq \mathrm{TdS}$

$$
\begin{equation*}
d q=d V+P d V \tag{iii}
\end{equation*}
$$

subsitituting value of dq from equation (iii) to equation (ii)

$$
\begin{array}{ll} 
& d V+P d V-T d S \leq 0 \\
\Rightarrow & d(H-T S)_{P, T} \leq 0 \\
\because & d(H-T S)_{P, T}^{-}=(d H-T d S-S d T)_{P, T} \\
= & (d U+P d V+V d P-T d S-S d T)_{P, T} \leq 0 \\
\Rightarrow & d(H-T S)_{P, T} \leq 0 \\
\Rightarrow & d(d G)_{P, T} \leq 0
\end{array}
$$

## Statement :

During course of every spontaneous process, Gibb's function decreases. If a process is allowed to run spontaneously, eventually it attain equilibrium. At equilibrium, the Gibb's function attains minimum value. No further decrease to the value of Gibb's function is possible at equilibrium.

$$
\text { Hence at equilibrium. }(\mathrm{dG})_{\mathrm{T}, \mathrm{P}}=0 \text {. }
$$

$\Rightarrow$ Entropy change in spontaneous process :

$$
\Delta \mathrm{S}_{\text {system }}+\Delta \mathrm{S}_{\text {surrounding }} \geq 0
$$

The sign > is for spontaneous process. A state of equilibrium in a close system is attained spontaneously. As system approaches equilibrium from non-equilibrium state $-\mathrm{S}_{\text {Total }}$ keeps on increasing and at equilibrium $\mathrm{S}_{\text {Total }}$ attains its maximum value.
$\Rightarrow \quad \Delta \mathrm{S}_{\text {Total }}=0$ at equilibrium
at this point $\quad S_{\text {Total }}=$ maximum value at equilibrium in a close system

## SIGNIFICANCE OF GIBB'S FUNCTION :

(a) Decrease in Gibb's function at constant temperature and pressure is related to $\Delta \mathrm{S}_{\text {total }}$ (total entropy change of system and surrounding).

We known :

$$
\text { also } \quad \begin{array}{ll}
\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{~S} & \ldots \ldots . .(\mathrm{i}) ; \text { at constant } \mathrm{T} \text { and pressure } \\
\Delta \mathrm{H}= & \mathrm{q}_{\mathrm{p}} \text { at constant pressure } \\
& \mathrm{q}_{\mathrm{p}}=\text { heat absorbed by system at constant pressure. } \tag{ii}
\end{array}
$$

$\Rightarrow \quad \Delta \mathrm{G}=\mathrm{q}_{\mathrm{p}}-\mathrm{T} \Delta \mathrm{S}$
this gives $-\frac{\Delta G}{T}=-\frac{q_{p}}{T}+\Delta S$

$$
-\frac{\mathrm{q}_{\mathrm{P}}}{\mathrm{~T}}+\Delta \mathrm{S}_{\text {surrounding }}
$$

$$
\Rightarrow \quad-\frac{\Delta \mathrm{G}}{\mathrm{~T}}=\left(\Delta \mathrm{S}_{\text {surrounding }}+\Delta \mathrm{S}_{\text {system }}\right)
$$

Student might get confused in

$$
\begin{aligned}
\text { ex : } & -\frac{\mathrm{q}}{\mathrm{~T}}=\Delta \mathrm{S}_{\text {surr. }} \\
\text { ex : } & \mathrm{q}=\text { Heat absorbed by system } \\
& -\mathrm{q}=\text { Heat absorbed by surrounding } \\
\Rightarrow & \\
& -\Delta \mathrm{G}=\mathrm{T}\left(\Delta \mathrm{~S}_{\text {Total }}\right)
\end{aligned}
$$

Note equation (ii) can be written as $\Delta \mathrm{G}=\mathrm{q}-\mathrm{q}_{\mathrm{rev}}$.
for spontaneous process $(\Delta \mathrm{G})_{T, \mathrm{P}}<0$
$\Rightarrow \mathrm{q}-\mathrm{q}_{\mathrm{rev}}<0 \Rightarrow \mathrm{q}_{\mathrm{rev}}>\mathrm{q}$
Gibbs function and non PV work :
Decrease in Gibb's function at constant temperature and pressure in a process gives an estimate or measure of maximum non-PV work which can be obtained from system in reversible, manner.
The example of non-PV work is electrical work done by chemical battery.
Expansion of soap bubble at for a closed system capable of doing non-PV work apart from PV work first law can be written as

$$
\mathrm{dU}=\mathrm{dq}-\mathrm{PdV}=\mathrm{dw}_{\mathrm{non}-\mathrm{PV}}
$$

$-\mathrm{dw}_{\text {non-PV }}=$ non-PV work done by the system.
$\mathrm{dG}=\mathrm{d}(\mathrm{H}-\mathrm{TS})$
$=\mathrm{dH}-\mathrm{TdS}-\mathrm{SdT}$
$d G=d U+P d V+V d P-T d S-S d T$
$\mathrm{dG}=\mathrm{dq}-\mathrm{PdV}-\mathrm{w}_{\text {non }, \mathrm{PV}}+\mathrm{PdV}+\mathrm{VdP}-\mathrm{TdS}-\mathrm{SdT}$
for a reversible change at cont. T and P

$$
\begin{array}{ll} 
& \mathrm{dG}=\mathrm{dq}_{\text {rev. }}-\mathrm{dw}_{\text {non }}+\mathrm{VdP}-\mathrm{TdS}-\mathrm{SdT} \\
\text { since } & \mathrm{dq}_{\text {rev }}=\mathrm{TdS} \\
\Rightarrow & -(\mathrm{dG})_{T, P}=\mathrm{dw}_{\text {non-Pv }}
\end{array}
$$

- Non-pV work is work done due to chemical energy transformation or due to composition change and decrease in Gibb's function in a isothermal and isobaric process provide a measure of chemical energy stored in bonds and intermolecular interaction energy of molecules.

Gibbs free energy change at constant temperature :
In order to derive an equation which will enable us to calculate the Gibbs free energy change of an isothermal process but with varying pressure, we may conveniently start with the equation,

$$
G=E+P V-T S
$$

Differentiating the above equation, we get

$$
\mathrm{dG}=\mathrm{dE}+\mathrm{PdV}+\mathrm{VdP}-\mathrm{TdS}-\mathrm{SdT}
$$

According to first law of thermodynamics,

$$
\begin{aligned}
\mathrm{dQ} & =\mathrm{dE}+\mathrm{PdV} \\
\therefore \quad \mathrm{dG} & =\mathrm{dQ}+\mathrm{VdP}-\mathrm{TdS}-\mathrm{SdT}
\end{aligned}
$$

Further since $\frac{d Q}{T}=d S$, we can replace $d Q$ by $T d$.
$\therefore \quad \mathrm{dG}=\mathrm{VdP}-\mathrm{SdT}$
At constant temperature, $\mathrm{dT}=0$
$\therefore \quad \mathrm{dG}=\mathrm{VdP}$
or $\left(\frac{d G}{d P}\right)_{r}=V$
Thus Gibb's function of every substance increases on increasing pressure, but this increase is maximum for gases, compared to solids or liquids since gases have maximum molar volume. On intergrating equation $\mathrm{dG}=\mathrm{VdP}$ for very minute changes from state 1 to 2 , we have

$$
\Delta \mathrm{G}=\mathrm{G}_{2}-\mathrm{G}_{1}=\int_{1}^{2} \mathrm{VdP}
$$

In case of one mole of a perfect gas,

$$
\begin{aligned}
& V=\frac{R T}{P} \\
\therefore \quad & \Delta G=R T \int_{1}^{2} \frac{d P}{P}=R T \ln \frac{\mathrm{P}_{2}}{\mathrm{P}_{1}}
\end{aligned}
$$

For n moles of a perfect gas, the free energy change is

$$
\Delta G=n R T \ln \frac{P_{2}}{P_{1}}
$$

- Gibbs free energy change at constant pressure

From equation which is

$$
\mathrm{dG}=\mathrm{VdP}-\mathrm{SdT} \quad \text { (Only for pure substances) }
$$

when pressure is constant, $\mathrm{dP}=0$
$\therefore \quad \mathrm{dG}=-\mathrm{SdT}$
or $\left(\frac{d G}{d T}\right)_{p}=-S$
thus Gibb's function of every substance decreases with temperature, but this decrease is maximum for gases since they have maximum state of disorder. Hence on increasing temperature, gas phase gain maximum stability compared to solid or liquid phase.
For chemical reaction :

$$
\mathrm{d}\left(\Delta_{\mathrm{r}} \mathrm{G}\right)=\Delta_{\mathrm{r}} \mathrm{~V}(\mathrm{dp})-\Delta_{\mathrm{r}} \mathrm{~S}(\mathrm{dT})
$$

at constant temperature, If $\Delta_{\mathrm{r}} \mathrm{V} \sim$ constant
$\Rightarrow \quad \int_{1}^{2} \mathrm{~d}\left(\Delta_{\mathrm{r}} \mathrm{C}_{\mathrm{p}}\right)=\Delta_{\mathrm{r}} \mathrm{V} \int_{1}^{2} \mathrm{dp}$

$$
\Rightarrow \quad \Delta_{\mathrm{r}} \mathrm{C}_{\mathrm{p}_{2}}-\Delta_{\mathrm{r}} \mathrm{C}_{\mathrm{p}_{1}}=\Delta_{\mathrm{r}} \mathrm{~V}\left(\mathrm{P}_{2}-\mathrm{P}_{1}\right)
$$

only for condensed phase : equilibrium like
$\mathrm{H}_{2} \mathrm{O}(\mathrm{s}) \rightleftharpoons \mathrm{H}_{2} \mathrm{O}(\ell)$
S (Rhombic) $\rightleftharpoons \mathrm{S}$ (monoclinic)

- GIBBS FREE ENERGY CHANGE IN CHEMICAL REACTIONS :

Gibbs free energy changes have a direct relationship with the tendency of the system to proceed to a state of equilibrium. In view of this fact, it is desirable to have a knowledge of the free energy of chemical compounds so that the Gibbs free energy change of a possible reaction could be easily calculated. Standard free energies have been used for this case. A zero value of the Gibbs free energy is assigned to the free energies of the stable form of the elements at 25 C and 1 atm . pressure.

With this as reference point, free energies of compounds have been calculated which are called standard Gibbs free energies of formation. The difference in the Gibbs free energy of products and reactants in their standard states (at 25 C and 1 bar pressure) is denoted as $\Delta \mathrm{G}$.
In standard enthalpy and entropy values are available, $\Delta \mathrm{G}$ can be written from equation as,

$$
\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{~S}
$$

- GIBB'S FREE ENERGY IN CHEMICAL REACTIONS FROM GIBB'S FREE ENERGY OF FORMATION OF COMPOUNDS :

Consider a chemical reaction,
$a A+b B \rightarrow c C+d D$
The standard Gibb's free energy change $\Delta \mathrm{G}$ can be computed on the basis discussed above (i.e., by assigning zero value to the Gibbs free energy of the stable form of elements at 25 C and 1 bar pressure). With this as reference, the standard Gibbs free energy of the products and reactants can be determined. The standard Gibbs free energy change for the overall reaction can be evaluted as :

$$
\begin{aligned}
& \Delta \mathrm{G}=\sum \mathrm{G}_{\mathrm{f} \text { (products) }}^{\circ}-\sum \mathrm{G}_{\mathrm{f} \text { freactants) }}^{\circ} \\
= & \left(\mathrm{cG} \mathrm{G}_{\mathrm{c}}^{\circ}+\mathrm{dG}_{\mathrm{D}}^{\circ}\right)-\left(\mathrm{aG}_{\mathrm{A}}^{\circ}+\mathrm{bG}_{\mathrm{B}}^{\circ}\right)
\end{aligned}
$$

A negative sign of $\Delta \mathrm{G}$ will show that the reaction will proceed spontaneously.
note that $\Delta G^{\circ}$ can be defined at any temperature, at standard pressure of 1 bar

## - Reversible phase transitions and Gibb's free energy change :

During reversible phase transition which occurs at transition temperatures, Gibb's function change become zero, impling the fact that these processes are reversible processes.
at 373 K and 1 atm pressure $\Delta \mathrm{G}=0$ for $\mathrm{H}_{2} \mathrm{O}(\mathrm{l}) \rightarrow \mathrm{H}_{2} \mathrm{O}(\mathrm{g})$
at 273 K and 1 atm pressure $\Delta \mathrm{G}=0$ for $\mathrm{H}_{2} \mathrm{O}(\mathrm{s}) \rightarrow \mathrm{H}_{2} \mathrm{O}(\mathrm{l})$
Gibb's energy and equilibrium constant, an important topic taken up in chemical equilibrium.
Application of Gibb's function in decribing variation of vapour pressure, boiling and melting point with temperature is taken up in chemical equilibrium and liquid solutions variation of $G / T$ with temperature , has important implication in pridicting feasibitily of process at different temperatures. This gives Famous Gibb's Helmholtz equation taken up in electrochemistry.
$\square$ Topics of thermodynamics taken up in later chapters :
Application of :

- Gibb's function and non-PV work is taken in electrochemistry.
- Gibb's free energy and phase equilibrium taken in liquid solution.
- Gibb's function and position of equilibrium and relationship between $\Delta G$ and $K_{\text {eq }}$ taken up in chemical equilibrium.
- Variation of $\frac{G}{T}$ with temperature also called Gibb's helmholtz equation taken in electrochemistry.


## MEMORY TIPS

## First law of thermodynamics

For a finite change : $q=\Delta E-w=\Delta E-P \Delta V$
where q is heat given to system, $\Delta \mathrm{E}$ is change in internal energy and -w is work done by the system.

$$
\mathrm{dq}=\mathrm{dE}-\mathrm{dw}=\mathrm{dE}-\mathrm{PdV}
$$

Work done in an irreversible process

$$
\mathrm{w}=-\mathrm{P}_{\text {ext }} \quad \Delta \mathrm{V}=-\mathrm{P}_{\text {ext }} \quad\left(\mathrm{V}_{2}-\mathrm{V}_{1}\right)=-\mathrm{P}_{\text {ext }} \quad \mathrm{R}\left[\frac{\mathrm{P}_{1} \mathrm{~T}_{2}-\mathrm{P}_{2} \mathrm{~T}_{1}}{\mathrm{P}_{1} \mathrm{P}_{2}}\right]
$$

$\mathrm{P}_{\text {ext }}$ is the pressure against which volume changes from $\mathrm{V}_{1}$ to $\mathrm{V}_{2}$
Work done in reversible process, i.e., Maximum work
Isothermal conditions

$$
\begin{aligned}
& \mathrm{w}_{\mathrm{rev}}=-2.303 \mathrm{nRT} \log _{10}\left(\mathrm{~V}_{2} / \mathrm{V}_{1}\right) \\
& \mathrm{w}_{\mathrm{rev}}=-2.303 \mathrm{nRT} \log _{10}\left(\mathrm{P}_{1} / \mathrm{P}_{2}\right)
\end{aligned}
$$

$\mathrm{w}_{\mathrm{rev}}$ is maximum work done.
Adiabatic conditions

$$
\mathrm{w}_{\mathrm{rev}}=[\mathrm{nR} /(\gamma-1)]\left[\mathrm{T}_{2}-\mathrm{T}_{1}\right]
$$

$\gamma$ is poisson's ratio.
Also for adiabatic process, following conditions hold good :
$\mathrm{PV}^{\gamma}=$ constant
$\mathrm{T}^{\gamma} \mathrm{P}^{1-\gamma}=$ constant
$\mathrm{V}^{\gamma-1}=$ constant

- Heat capacities :

At constant pressure $\quad \mathrm{C}_{\mathrm{p}}=(\delta \mathrm{H} / \delta \mathrm{H})_{\mathrm{p}}$ $C_{p}$ is molar heat capacity at constant pressure.
At constant volume $\quad \mathrm{C}_{\mathrm{v}}=(\delta \mathrm{E} / \delta \mathrm{T})_{\mathrm{v}}$
$\mathrm{C}_{\mathrm{v}}$ is molar heat capacity at constant volume.

$$
C_{p} \quad c_{p} \quad M \text { and } C_{v}=c_{v} \quad M
$$

and

$$
C_{p}-C_{v}=R / M
$$

$$
\mathrm{C}_{\mathrm{p}} / \mathrm{C}_{\mathrm{v}}=\mathrm{c}_{\mathrm{p}} / \mathrm{c}_{\mathrm{v}}=\gamma \quad \text { (The poisson's ratio) }
$$

$c_{p}$ and $c_{v}$ are specific heats at constant pressure and volume respectively.

- Entropy

$$
\begin{aligned}
& \Delta \mathrm{S}=\sum \mathrm{S}_{\text {products }}-\sum \mathrm{S}_{\text {reactants }} \\
& \Delta \mathrm{S}=\mathrm{q}_{\text {rev }} / \mathrm{T}=2.303 \mathrm{nR} \log _{10}\left(\mathrm{~V}_{2} / \mathrm{V}_{1}\right)=2.303 \mathrm{nR} \log _{10}\left(\mathrm{P}_{1} / \mathrm{P}_{2}\right) \\
& \Delta \mathrm{S}_{\text {fusion }}=\Delta \mathrm{H}_{\text {fusion }} / \mathrm{T} \\
& \Delta \mathrm{~S}_{\text {vap }}=\Delta \mathrm{H}_{\text {vap }} / \mathrm{T}
\end{aligned}
$$

$\Delta \mathrm{S}$ is entropy change.

Free energy
$G=H-T S$
$\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{S}$ and $\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{S} \quad$ (In standard state)
At equilibrium, $\Delta \mathrm{G}=0$
$-\Delta G=R T \ln K_{p}\left(\right.$ or $\left.K_{C}\right)$
$=2.303 \mathrm{RT} \log _{10} \mathrm{~K}_{\mathrm{p}}\left(\right.$ or $\left.\mathrm{K}_{\mathrm{C}}\right)$
$\Delta G$ is free energy change and $\Delta G$ is standard free energy change. $K_{C}$ and $K_{p}$ are equilibrium constants in terms of concentration and pressure respectively.

- Unit conversion

$$
\begin{aligned}
& 1 \mathrm{cal}=4.1868 \mathrm{~J}=4.1868 \quad 10^{7} \text { erg. } \\
& 1 \mathrm{~J}=10^{7} \text { ergs } \\
& 1 \mathrm{eV}=1.602 \quad 10^{-19}=1.602 \quad 10^{-12} \text { ergs. } \\
& 1 \mathrm{MeV}=10^{6} \mathrm{eV} \\
\text { order }: & 1 \mathrm{cal}>1 \mathrm{~J}>1 \text { erg }>1 \mathrm{eV} .
\end{aligned}
$$

## SOLVED EXAMPLES

Ex. 1 During 200J work done on the system, 140 J of heat is given out. Calculate the change in internal energy.
Sol. $\quad w=200 \mathrm{~J} ; \quad \mathrm{q}=-140 \mathrm{~J}$;
$\because \quad q=\Delta E+(-w)$; where $-w$ is work done by the system

$$
\begin{aligned}
& \Delta \mathrm{E}=\mathrm{q}+\mathrm{w} \\
& \Delta \mathrm{E}=-140+200=+60 \mathrm{~J}
\end{aligned}
$$

Ex. 2 A gas absorbs 200 J of heat and expands against the external pressure of 1.5 atm from a volume of 0.5 litre. Calculate the change in internal energy.

Sol. $\quad w=-P \Delta V=-1.5 \quad(1.0-0.5)=-0.75$ litre atm

$$
=-0.75 \quad 101.3 \mathrm{~J}=-75.975 \mathrm{~J}
$$

$\because \quad 1$ litre atm $=101.3 \mathrm{~J}$
Now, $\quad \Delta \mathrm{E}=200-75.975=+124.025 \mathrm{~J}$
Ex. 3 Two litre of $\mathrm{N}_{2}$ at $0^{\circ} \mathrm{C}$ and 5 atm pressure are expanded isothermally against a constant external pressure of 1 atm until the pressure of gas reaches 1 atm . Assuming gas to be ideal, calculate work of expansion.
Sol. Since the external pressure is greatly different from the pressure of $\mathrm{N}_{2}$ and thus, process is irreversible.

$$
\begin{aligned}
& \mathrm{w}=-\mathrm{P}_{\text {ext }}\left(\mathrm{V}_{2}-\mathrm{V}_{1}\right) \\
& \mathrm{w}=-1 \quad\left(\mathrm{~V}_{2}-\mathrm{V}_{1}\right)
\end{aligned}
$$

$$
\text { Given } \mathrm{V}_{1}=2 \text { litre } \quad \mathrm{V}_{2}=? \mathrm{~T}=273 \mathrm{~K}
$$

$$
\mathrm{P}_{1}=5 \mathrm{~atm} \quad \mathrm{P}_{2}=1 \mathrm{~atm}
$$

$$
\therefore \quad \mathrm{P}_{1} \mathrm{~V}_{1}=\mathrm{P}_{2} \mathrm{~V}_{2}
$$

$$
\therefore \quad V_{2}=\frac{2 \times 5}{1}=10 \text { litre }
$$

$$
\therefore \quad w=-1 \quad(10-2)=-8 \text { litre atm }
$$

$$
\therefore \quad=-\frac{8 \times 1.987}{0.0821} \text { calorie }=-\frac{8 \times 1.987 \times 4.184}{0.0821} \mathrm{~J}=-810.10 \text { joule }
$$

Ex. 4 The enthalpy of vaporisation of liquid diethyl ether $-\left(\mathrm{C}_{2} \mathrm{H}_{5}\right)_{2} \mathrm{O}$, is $26.0 \mathrm{~kJ} \mathrm{~mol}^{-1}$ at its boiling point $\left(35.0^{\circ} \mathrm{C}\right)$. Calculate $\Delta \mathrm{S}$ for conversion of : (a) liquid to vapour, and (b) vapour to liquid at $35^{\circ} \mathrm{C}$.

Sol. (a) $\Delta \mathrm{S}_{\text {vap. }}=\frac{\Delta \mathrm{H}_{\text {vap. }}}{\mathrm{T}}=\frac{26 \times 10^{3}}{308}=+84.41 \mathrm{JK}^{-1} \mathrm{~mol}^{-1}$
(b) $\Delta \mathrm{S}_{\text {cond. }}=\frac{\Delta \mathrm{H}_{\text {cond. }}}{\mathrm{T}}=-\frac{26 \times 10^{3}}{308} \quad\left(\because \mathrm{H}_{\text {cond }}=-26 \mathrm{~kJ}\right)$

$$
=-84.41 \mathrm{JK}^{-1} \mathrm{~mol}^{-1}
$$

Ex. 5 Calculate the free energy change when 1 mole of NaCl is dissolved in water at $25^{\circ} \mathrm{C}$. Lattice energy of NaCl $=777.8 \mathrm{~kJ} \mathrm{~mol}^{-1} ; \Delta \mathrm{S}$ for dissolution $=0.043 \mathrm{~kJ} \mathrm{~mol}^{-1}$ and hydration energy of $\mathrm{NaCl}=-774.1 \mathrm{~kJ} \mathrm{~mol}{ }^{-1}$.

Sol. $\Delta \mathrm{H}_{\text {dissolution }}=$ Lattice energy + Hydration energy

$$
=777.8-774.1=3.7 \mathrm{~kJ} \mathrm{~mol}^{-1}
$$

Now $\quad \Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{S}$

$$
=3.7-298 \quad 0.043=3.7-12.814
$$

$$
\Delta \mathrm{G}=-9.114 \mathrm{~kJ} \mathrm{~mol}^{-1}
$$

Ex. 6 The equilibrium constant for the reaction given below is $2.0 \quad 10^{-7}$ at 300 K . Calculate the standard free energy change for the reaction;

$$
\mathrm{PCl}_{5(\mathrm{~g})} \rightleftharpoons \mathrm{PCl}_{3(\mathrm{~g})}+\mathrm{Cl}_{2(\mathrm{~g})}
$$

Also, calculate the standard entropy change if $\Delta \mathrm{H}^{\circ}=28.40 \mathrm{~kJ} \mathrm{~mol}{ }^{-1}$.
Sol. $\quad \Delta G^{0}=-2.303 \quad 8.314 \quad 300 \log \left[\begin{array}{lll}2.0 & 10^{-7}\end{array}\right]$

$$
=+38479.8 \mathrm{~J} \mathrm{~mol}^{-1}=+38.48 \mathrm{~kJ} \mathrm{~mol}^{-1}
$$

Also, $\Delta \mathrm{G}^{0}=\Delta \mathrm{H}^{0}-\mathrm{T} \Delta \mathrm{S}^{\circ}$

$$
\begin{aligned}
\therefore \quad \Delta \mathrm{S}^{\circ}= & \frac{\Delta \mathrm{H}^{\circ}-\Delta \mathrm{G}^{\circ}}{\mathrm{T}}=\frac{28.40-38.48}{300} \\
& =-0.0336 \mathrm{~kJ}=-33.6 \mathrm{JK}^{-1}
\end{aligned}
$$

Ex. 7 One mole of a perfect monoatomic gas is put through a cycle consisting of the following three reversible steps :

(CA) Isothermal compression from 2 atm and 10 litres to 20 atm and 1 litre.
(AB) Isobaric expansion to return the gas to the original volume of 10 litres with $T$ going from $T_{1}$ to $T_{2}$.
(BC) Cooling at constant volume to bring the gas to the original pressure and temperature.
The steps are shown schematically in the figure shown.
(a) Calculate $T_{1}$ and $T_{2}$.
(b) Calculate $\Delta \mathrm{E}, \mathrm{q}$ and w in calories, for each step and for the cycle.

Sol. We know,
Path CA - Isothermal compression
Path AB - Isobaric expansion
Path BC - Isochoric change
Let $V_{i}$ and $V_{f}$ are initial volume and final volume at respective points,
For temperature $\mathrm{T}_{1}$ (For C ): $\quad \mathrm{PV}=\mathrm{nRT}_{1}$

$$
\begin{array}{ccc} 
& 2 & 10=10.0821 \\
\mathrm{~T}_{1} \\
\therefore & \mathrm{~T}_{1}=243.60 \mathrm{~K} &
\end{array}
$$

For temperature $T_{2}$ (For $C$ and B) : $\frac{P_{1} V_{1}}{T_{1}}=\frac{P_{2} V_{2}}{T_{2}}$

$$
\begin{array}{ll} 
& \frac{2 \times 10}{\mathrm{~T}_{1}}=\frac{20 \times 10}{\mathrm{~T}_{2}} \\
\therefore & \frac{\mathrm{~T}_{2}}{\mathrm{~T}_{1}}=10 \\
\therefore & \mathrm{~T}_{2}=243.60 \quad 10=2436.0 \mathrm{~K}
\end{array}
$$

Path CA: w $=+2.303 n R T_{1} \log \frac{V_{i}}{V_{f}}$

$$
\begin{aligned}
& =2.303 \\
& 1
\end{aligned} 22 \quad 243.6 \log \frac{10}{1}
$$

$\Delta \mathrm{E}=0$ for isothermal compression ; Also $\mathrm{q}=\mathrm{w}$
Path $A B: \quad w=-P\left(V_{f}-V_{i}\right)$

$$
\begin{aligned}
& =-20 \quad(10-1)=-180 \text { litre atm } \\
& =\frac{-180 \times 2}{0.0821}=-4384.9 \mathrm{cal}
\end{aligned}
$$

Path BC: w $=-\mathrm{P}\left(\mathrm{V}_{\mathrm{f}}-\mathrm{V}_{\mathrm{i}}\right)=0 \quad\left(\because \mathrm{~V}_{\mathrm{f}}-\mathrm{V}_{\mathrm{i}}=0\right)$
since volume is constant for monoatomic gas heat change at constant volume $=q_{v}=\Delta \mathrm{E}$.
Thus for path $B C \quad q_{v}=C_{v} \quad n \quad \Delta T=\Delta E$

$$
\begin{aligned}
\therefore \quad \mathrm{q}_{\mathrm{v}} & =\frac{3}{2} R \quad 1 \quad(2436-243.6) \\
\mathrm{q}_{\mathrm{v}} & =\frac{3}{2} \quad 2
\end{aligned} 1 \quad 2192.4=6577.2 \mathrm{cal} \text { l }
$$

Since process involves cooling $\quad \therefore \quad \mathrm{q}_{\mathrm{v}}=\Delta \mathrm{E}=-6577.2 \mathrm{cal}$
Also in path $A B$, the intenal energy in state $A$ and state $C$ is same. Thus during path $A B$, an increase in internal energy equivalent of change in internal energy during path BC should take place. Thus $\Delta \mathrm{E}$ for path $\mathrm{AB}=+6577.2 \mathrm{cal}$

Now q for path $A B=\Delta E-w_{A B}=6577.2+4384.9=10962.1 \mathrm{cal}$
Cycle : $\Delta \mathrm{E}=0 ; \quad \mathrm{q}=-\mathrm{w}=-\left[\mathrm{w}_{\text {Path } \mathrm{CA}}+\mathrm{w}_{\text {Path } A B}+\mathrm{w}_{\text {Path } \mathrm{BC}}\right]$

$$
=-[+1122.02+-4384.9+0]
$$

$\therefore \quad \mathrm{q}=-\mathrm{w}$

$$
=+3262.88 \mathrm{cal}
$$

Ex. 8 A monoatomic ideal gas of two moles is taken through a cyclic process starting from A as shown in figure.
The volume ratios are $\frac{\mathrm{V}_{\mathrm{B}}}{\mathrm{V}_{\mathrm{A}}}=2$ and $\frac{\mathrm{V}_{\mathrm{D}}}{\mathrm{V}_{\mathrm{A}}}=4$. If the temperature $\mathrm{T}_{\mathrm{A}}$ at A is $27^{\circ} \mathrm{C}$, calculate :

(a) The temperature of the gas at point B .
(b) Heat absorbed or released by the gas in each process.
(c) The total work done by the gas during complete cycle.

Sol. For the given cyclic process,

$$
\frac{V_{B}}{V_{A}}=2, \quad \frac{V_{D}}{V_{A}}=4, \quad T_{A}=300 \mathrm{~K}
$$

(a) For isobaric process $A B$

$$
\begin{aligned}
& \frac{\mathrm{V}_{A}}{T_{A}}=\frac{\mathrm{V}_{B}}{T_{B}} \\
\therefore \quad & \mathrm{~T}_{B}=T_{A} \quad \frac{V_{B}}{V_{A}}=300 \quad 2=600 \mathrm{~K}
\end{aligned}
$$

(b) The following process are there in complete cycle
(i) $\mathrm{A} \rightarrow \mathrm{B}$ Isobaric expansion
(ii) $\mathrm{B} \rightarrow \mathrm{C}$ Isothermal expansion
(iii) $\mathrm{C} \rightarrow \mathrm{D}$ Isochoric compression
(iv) $\mathrm{D} \rightarrow \mathrm{A}$ Isothermal compression

For (i) $\mathrm{q}_{\mathrm{A} \rightarrow \mathrm{B}}=+\mathrm{n} \quad \mathrm{C}_{\mathrm{P}} \quad \Delta \mathrm{T}=+2 \quad \frac{5}{2} \quad \mathrm{R} \quad 300=+1500 \quad 2=+3000 \mathrm{cal}(\mathrm{R}=2 \mathrm{cal})$
(ii) $\mathrm{q}_{\mathrm{B} \rightarrow \mathrm{C}}=\Delta \mathrm{E}-\mathrm{w} \quad(\Delta \mathrm{E}=0)$
$\therefore \quad \mathrm{q}_{\mathrm{B} \rightarrow \mathrm{C}}=\Delta \mathrm{E}-\mathrm{w}=+\int \mathrm{PdV}=+\mathrm{nRT} \ln \frac{\mathrm{V}_{\mathrm{D}}}{\mathrm{V}_{\mathrm{B}}}=+2 \times 2 \times 600 \ln \frac{4}{2}=+1.663+10^{3} \mathrm{cal}$
(iii) $\quad \mathrm{q}_{\mathrm{C} \rightarrow \mathrm{D}}=\mathrm{n} \quad \mathrm{C}_{\mathrm{v}} \quad \Delta \mathrm{T}=2 \quad \frac{3}{2} \quad 2-300=-1800 \mathrm{cal}$
(iv) $\quad \mathrm{q}_{\mathrm{D} \rightarrow \mathrm{A}}=+n R T_{A} \ln \frac{\mathrm{~V}_{A}}{\mathrm{~V}_{\mathrm{D}}}=+2 \quad 2 \quad 300 \ln \frac{1}{4}=-2 \quad 2 \quad 300 \quad 1.386=-1.663 \quad 10^{3} \mathrm{cal}$
$\therefore \quad \mathrm{Q}=\mathrm{q}_{A \rightarrow B}+\mathrm{q}_{\mathrm{B} \rightarrow \mathrm{C}}+\mathrm{q}_{\mathrm{C} \rightarrow \mathrm{D}}+\mathrm{q}_{\mathrm{D} \rightarrow \mathrm{A}}=3000+1663-1800-1663=1200 \mathrm{cal}$
(c) Since the process ABCDA is a cyclic process

$$
\therefore \quad \Delta \mathrm{E}=0 \quad \text { or } \quad \mathrm{Q}=\Delta \mathrm{E}-\mathrm{Q}=-\mathrm{w} \text { or } \mathrm{Q}=-1200 \mathrm{cal}
$$

i.e., work done on the system $=1200 \mathrm{cal}$

Ex. 9 Calculate the work done when 50 g of iron reacts with hydrochloric acid in :
(i) a closed vessel of fixed volume,
(ii) an open beaker at 25 C .

Sol. We know,
(i) Vessel is of fixed volume, hence $\Delta \mathrm{V}=0$. No work is done, $\mathrm{w}=0$
(ii) The $\mathrm{H}_{2}$ gas formed drives back the atmosphere hence.

$$
\mathrm{w}=-\mathrm{P}_{\text {ext }} \cdot \Delta \mathrm{V}
$$

Also

$$
\Delta V=V_{\text {final }}-V_{\text {inititial }} \sim V_{\text {final }}\left(\because V_{\text {intital }}=0\right)
$$

$$
\therefore \quad \Delta \mathrm{V}=\frac{\mathrm{nRT}}{\mathrm{P}_{\text {ext }}}
$$

or $\quad w=-P_{\text {ext }} \cdot \frac{n R T}{P_{\text {ext }}}=-n R T$
where n is the number of mole of $\mathrm{H}_{2}$ gas obtained from n mole of $\mathrm{Fe}_{(s)}$.

$$
\begin{array}{ll} 
& \begin{array}{l}
\mathrm{Fe}_{(\mathrm{s})}=2 \mathrm{HCl}_{(\mathrm{aq})} \rightarrow \\
\\
1 \text { mole }
\end{array} \\
\therefore \quad & \mathrm{FeCl}_{2(\mathrm{aq} .)}+ \\
\therefore \quad \begin{array}{c}
\mathrm{H}_{2(\mathrm{~g})} \\
1 \text { mole }
\end{array} \\
\therefore \quad & \mathrm{n}=\frac{50}{56}=0.8929 \text { mole } \\
& \mathrm{w}=-0.8929 \quad 8.314 \quad 298 \\
& =-2212.22 \mathrm{~J}
\end{array}
$$

The reaction mixture in the given system does 2.212 kJ of work driving back to atmosphere.

Ex. 10 The internal energy change in the conversion of 1.0 mole of the calcite form of $\mathrm{CaCO}_{3}$ to the aragonite form is +0.21 kJ . Calculate the enthalpy change when the pressure is 1.0 bar ; given that the densities of the solids are $2.71 \mathrm{~g} \mathrm{~cm}^{-3}$ and $2.93 \mathrm{~g} \mathrm{~cm}^{-3}$ respectively.
Sol.

$$
\begin{array}{ll}
\text { Given } & \Delta \mathrm{E}=+0.21 \mathrm{~kJ} \mathrm{~mol}^{-1}=0.21 \quad 10^{3} \mathrm{~J} \mathrm{~mol}^{-1} \\
& \mathrm{P}=\overline{1}=1.0 \quad 10^{5} \mathrm{~Pa} \\
& \Delta \mathrm{~V}=\mathrm{V}_{\text {(aragonite) }}-\mathrm{V}_{\text {(Cacitit) }} \\
& =\left(\frac{100}{2.93}-\frac{100}{2.71}\right) \mathrm{cm}^{3} \mathrm{~mol}^{-1} \text { of } \mathrm{CaCO}_{3} \\
& =-2.77 \mathrm{~cm}^{3}=-2.77 \quad 10^{-6} \mathrm{~m}^{3} \\
\therefore \quad & \Delta \mathrm{H}=0.21 \quad 10^{3}-1 \quad 10^{5} \quad 2.77 \quad 10^{-6}=209.72 \mathrm{~J}=0.20972 \mathrm{~kJ} \mathrm{~mol}^{-1}
\end{array}
$$

Ex. 11 For a reaction $\mathrm{M}_{2} \mathrm{O}(\mathrm{s}) \rightarrow 2 \mathrm{M}(\mathrm{s})+\frac{1}{2} \mathrm{O}_{2}(\mathrm{~g}) ; \Delta \mathrm{H}=30 \mathrm{~kJ} \mathrm{~mol}^{-1}$ and $\Delta \mathrm{S}=0.07 \mathrm{~kJ} \mathrm{~K}^{-1} \mathrm{~mol}^{-1}$ at 1 atm . Calculate upto which temperature, the reaction would not be spontaneous.
Sol. Given, for the change, $\Delta \mathrm{H}=30 \quad 10^{3} \mathrm{~J} \mathrm{~mol}^{-1}, \Delta \mathrm{~S}=70 \mathrm{JK}^{-1} \mathrm{~mol}^{-1}$
For a non-spontaneous reaction

|  | $\Delta \mathrm{G}=+\mathrm{ve}$ |
| :--- | :--- |
| Since | $\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{S}$ |
| $\therefore$ | $\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{S}$ should be +ve |
| or | $\Delta \mathrm{H}>\mathrm{T} \Delta \mathrm{S}$ |
| or | $\mathrm{T}<\frac{\Delta H}{\Delta \mathrm{~S}} \Rightarrow \mathrm{~T}<\frac{30 \times 10^{3}}{70} \Rightarrow \mathrm{~T}<428.57 \mathrm{~K}$ |

Ex. 12 Predict whether the entropy change of the system in each of the following process is positive or negative.
(a) $\mathrm{CaCO}_{3}(\mathrm{~s}) \rightarrow \mathrm{CaO}$ (s) $+\mathrm{CO}_{2}(\mathrm{~g})$
(b) $\mathrm{N}_{2}(\mathrm{~g})+3 \mathrm{H}_{2}(\mathrm{~g}) \rightarrow 2 \mathrm{NH}_{3}(\mathrm{~g})$
(c) $\mathrm{N}_{2}(\mathrm{~g})+\mathrm{O}_{2}(\mathrm{~g}) \rightarrow 2 \mathrm{NO}(\mathrm{g})$
(d) $\mathrm{HCl}(\mathrm{g})+\mathrm{NH}_{3}(\mathrm{~g}) \rightarrow \mathrm{NH}_{4} \mathrm{Cl}(\mathrm{s})$
(e) $2 \mathrm{SO}_{2}(\mathrm{~g})+\mathrm{O}_{2}(\mathrm{~g}) \rightarrow 2 \mathrm{SO}_{3}(\mathrm{~g})$
(f) Cooling of $\mathrm{N}_{2}(\mathrm{~g})$ from 20 C to -50 C

Sol. Gaseous substances generally possess more entropy than solids. So whenever the products contain more moles of a gas than the reactants, the entropy change is probably positive. And hence, $\Delta \mathrm{S}$ is
(a) positive
(b) negative
(c) small, the sign of $\Delta \mathrm{S}$ is impossible to predict
(d) negative
(e) negative
(f) negative
[Note : For a given substance at a given temperature, $\mathrm{S}_{\text {gas }}>\mathrm{S}_{\text {liquid }}>\mathrm{S}_{\text {solid }}$ ]
Ex. 13 Calculate the boiling point of bromine from the following data :
$\Delta \mathrm{H}^{\circ}$ and $\Delta \mathrm{S}^{\circ}$ values of $\mathrm{Br}_{2}(\mathrm{l}) \rightarrow \mathrm{Br}_{2}(\mathrm{~g})$ are $30.91 \mathrm{~kJ} / \mathrm{mole}$ and $93.2 \mathrm{~J} / \mathrm{mol}$. K respectively. Assume that $\Delta \mathrm{H}$ and $\Delta \mathrm{S}$ do not vary with temperature.
Sol. Consider the process: $\mathrm{Br}_{2}(\mathrm{l}) \rightarrow \mathrm{Br}_{2}(\mathrm{~g})$
The b.p. of a liquid is the temperature at which the liquid and the pure gas coexist at equilibrium at 1 atm .

$$
\therefore \quad \Delta \mathrm{G}=0
$$

As it is given that $\Delta \mathrm{H}$ and $\Delta \mathrm{S}$ do not change with temperature

$$
\begin{aligned}
& \Delta \mathrm{H}=\Delta \mathrm{H}=30.91 \mathrm{~kJ} \\
& \Delta \mathrm{~S}=\Delta \mathrm{S}=93.2 \mathrm{~J} / \mathrm{K}=0.0932 \mathrm{~kJ} / \mathrm{K}
\end{aligned}
$$

We have, $\Delta \mathrm{G}=\Delta \mathrm{H}-\mathrm{T} \Delta \mathrm{S}=0$
$\therefore \quad \mathrm{T}=\frac{\Delta \mathrm{H}}{\Delta \mathrm{S}}=\frac{30.91}{0.0932}=331.6 \mathrm{~K}$.
This is the temperature at which the system is in equilibrium, that is, the b.p of bromine.

Ex. 14 The efficiency of the Carnot engine is $1 / 6$. On decreasing the temperature of the sink by 65 K , the efficiency increases to $1 / 3$. Find the temperature of the source and the sink.
Sol. We have,

$$
\begin{align*}
& \eta \\
& =\frac{T_{2}-T_{1}}{T_{2}} \text {, where } T_{1} \text { and } T_{2} \text { are the temperatures of sink and source respectively. }  \tag{i}\\
\therefore \quad \eta & =\frac{T_{2}-T_{1}}{T_{2}}=\frac{1}{6}
\end{align*}
$$

Now the temperature of the sink is reduced by 65 K .
$\therefore \quad$ temp. of the sink $=\left(\mathrm{T}_{1}-65\right)$
$\therefore \quad \eta=\frac{T_{2}-\left(T_{1}-65\right)}{T_{2}}=\frac{1}{3}$
On solving eqns. (i) and (ii), we get,

$$
\begin{aligned}
& \mathrm{T}_{1}=325 \mathrm{~K} \\
& \mathrm{~T}_{2}=390 \mathrm{~K}
\end{aligned}
$$

Ex. 15 (a) One mole of an ideal gas expands isothermally and reversible at $25^{\circ} \mathrm{C}$ from a volume of 10 litres to a volume of 20 litres.
(i) What is the change in entropy of the gas ?
(ii) How much work is done by the gas ?
(iii) What is q(surroundings) ?
(iv) What is the change in the entropy of the surroundings ?
(v) What is the change in the entropy of the system plus the surroundings ?
(b) Also answer the questions (i) to (v) if the expansion of the gas occurs irreversibly by simply opening a stopcock and allowing the gas to rush into an evacuated bulb of $10-\mathrm{L}$ volume.

Sol. (i) $\Delta \mathrm{S}=2.303 \mathrm{nR} \log \frac{\mathrm{V}_{2}}{\mathrm{~V}_{1}}=2.303 \quad 1 \quad 8.314 \quad \log \frac{20}{10}=5.76 \mathrm{~J} / \mathrm{K}$.
(a) (ii) $\mathrm{w}_{\text {rev }}=2.303 \mathrm{nRT} \log \frac{\mathrm{V}_{2}}{\mathrm{~V}_{1}}$

$$
=-2.303 \quad 1 \quad 8.314 \quad 298 \quad \log \frac{20}{10}=-1718 \mathrm{~J}
$$

(iii) For isothermal process, $\Delta \mathrm{E}=0$ and heat is absorbed by the gas,

$$
\begin{aligned}
& \mathrm{q}_{\mathrm{rev}}=\Delta \mathrm{E}-\mathrm{W}=0-(-1718)=1718 \mathrm{~J} \\
\therefore \quad & \mathrm{q}_{\text {surr }}=1718 \mathrm{~J} . \quad(\because \text { process is reversible })
\end{aligned}
$$

(iv) $\Delta \mathrm{S}_{\text {surr }}=-\frac{1718}{298}=-5.76 \mathrm{~J} / \mathrm{K}$.

As entropy of the system increases by 5.76 J , the entropy of the surroundinig decreases by 5.76 J , since the process is carried out reversible.
(v) $\Delta \mathrm{S}_{\text {sys }}+\Delta \mathrm{S}_{\text {surr }}=0 \ldots \ldots$. for reversible process.
(b) (i) $\Delta \mathrm{S}=5.76 \mathrm{~J} / \mathrm{K}$, which is the same as above because S is a state function.
(ii) $\mathrm{w}=0 . \quad\left(\because \mathrm{p}_{\text {ext }}=0\right)$
(iii) No heat is exchanged with the surroundings.
(iv) $\Delta \mathrm{S}_{\text {surr }}=0$
(v) The entropy of the system plus surroundings increases by $5.76 \mathrm{~J} / \mathrm{K}$, as we expect entropy to increases in an irreversible process.

